

Modeling of straight jet dynamics in electrospinning of polymer nanofibers

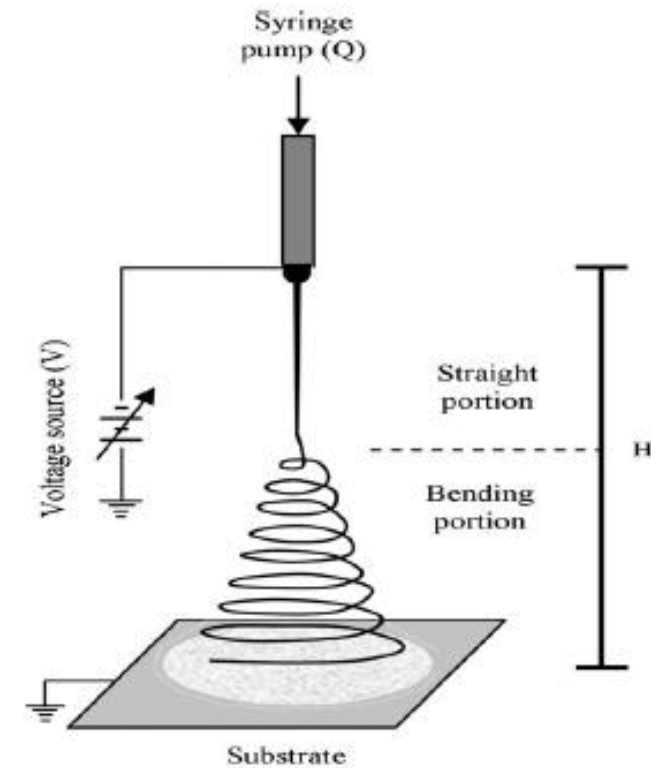
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Introduction

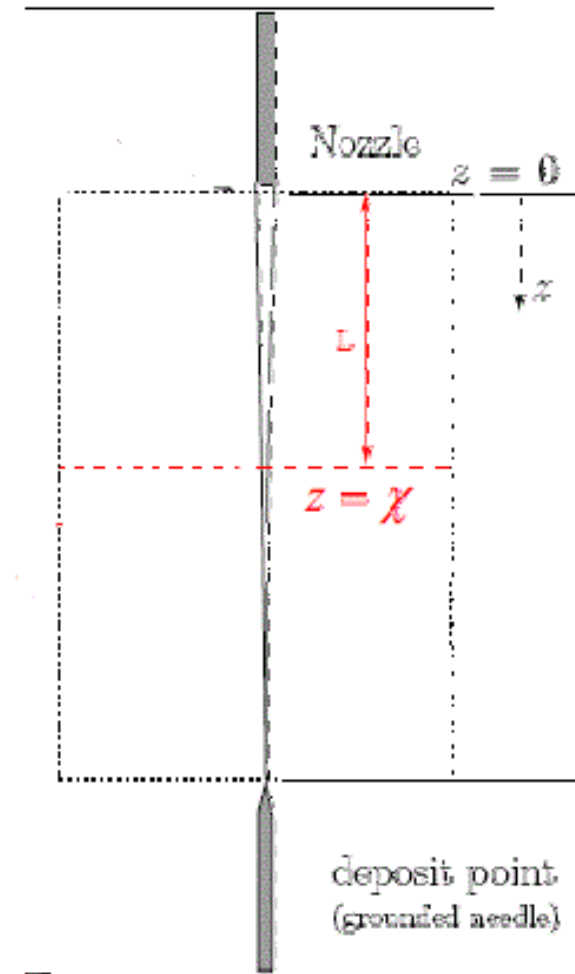
- Nanofibers are produced by solidification of a polymer solution stretched by an electric field.
- Properties:
 - High surface area per unit mass,
 - Very high porosity,
 - Layer thinness,
 - High permeability,
 - Low basic weight,
- Applications:
 - wound dressing,
 - drug or gene delivery vehicles, biosensors,
 - fuel cell membranes and electronics,
 - tissue-engineering processes.



Mathematical modeling in electrospinning process of nanofibers: a detailed review- S. Rafiei, S. Maghsoodloo, B. Noroozi, Mottaghtalab and A. K. Haghi(2012)

Objective

- Build a mathematical model to predict the **radius** of a straight jet electrospinning process.
- Validate the model for
 - Newtonian fluid
 - Non Newtonian fluid
 - Viscoelastic fluid
- Study the dependence of radius on various working parameters.



Basic Assumptions

- Slender body theory
 - $R(z) \propto z^{-1/4}$
 - $R + 4zR' = 0$
- Leaky dielectric model
 - Free charge which accumulates on the interface modifies the field.
 - Viscous flow develops - stresses balance the tangential components of the field acting on interface charge
- Laminar flow
- Electric field inside the fibre is being solved

Mathematical Model

- Mass conservation equation:

$$-\pi R^2 v = Q$$

- charge conservation equation:

$$-\pi R^2 KE + 2\pi R v \sigma = I$$

- Electric Field equation:

$$-E(z) = E_\infty(z) - \ln \chi \left(\frac{1}{\bar{\epsilon}} \frac{d(\sigma R)}{dz} - \frac{\beta}{2} \frac{d^2(ER^2)}{dz^2} \right)$$

- Momentum Equation:

$$-\frac{d(\pi R^2 \rho v^2)}{dz} = \pi R^2 \rho g + \frac{d[\pi R^2 (-p + \tau_{zz})]}{dz} + \frac{\gamma}{R} 2\pi R R' + 2\pi R (t_t^e - t_n^e R')$$

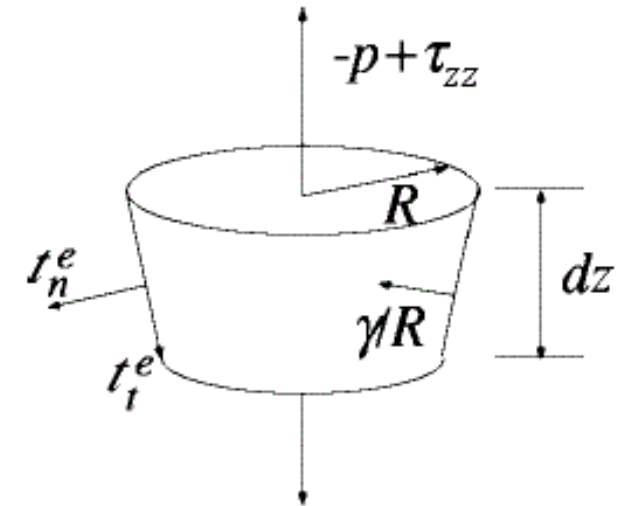


FIG. 1. Momentum balance on a short section of the jet.

Characteristic Scales

Length: R_0

Velocity: $v_0 = Q / (\rho R_0^2)$

Electric field: $E_0 = I / (\rho R_0^2 K)$

Surface charge density: $\sigma_0 = \bar{\epsilon} E_0$

Stress: $\tau_0 = \eta_0 v_0 / R_0$

Dimensionless groups:

Froude number: $Fr = \frac{v_0^2}{gR_0}$,

Reynolds number: $Re = \frac{\rho v_0 R_0}{\eta_0}$,

Weber number: $We = \frac{\rho v_0^2 R_0}{\gamma}$,

Deborah number: $De = \frac{\lambda v_0}{R_0}$,

viscosity ratio: $r_\eta = \frac{\eta_p}{\eta_0}$,

aspect ratio: $\chi = \frac{L}{R_0}$,

Electric Peclet number: $Pe = \frac{2\bar{\epsilon}v_0}{KR_0}$,

Electrostatic force parameter: $\varepsilon = \frac{\bar{\epsilon}E_0^2}{\rho v_0^2}$,

Dielectric constant ratio: $\beta = \frac{\epsilon}{\bar{\epsilon}} - 1$,

Mathematical Model (non-dimensional)

- Mass conservation equation:

$$-R^2 v = 1$$

- Charge conservation equation:

$$-ER^2 + PeRv\sigma = 1$$

- Electric Field equation:

$$-E = E_\infty - \ln \chi \left(\frac{d(\sigma R)}{dz} - \frac{\beta}{2} \frac{d^2(ER^2)}{dz^2} \right)$$

- Momentum Equation:

$$-vv' = \frac{1}{Fr} + \frac{T'}{ReR^2} + \frac{R'}{WeR^2} + \varepsilon \left(\sigma\sigma' + \beta EE' + \frac{2E\sigma}{R} \right)$$

Tensile Force,

$T = 3\eta R^2 v'$, for Newtonian and Non-Newtonian

$T = T'_p + 3\eta(1 - r_\eta)R^2 v'$, for viscoelastic fluids.

Polymer Stress Tensor Equation (Giesekus viscoelastic fluid)

$$\tau_{prr} + \lambda(v\tau'_{prr} + v' \tau_{prr}) + \alpha \frac{\lambda}{\eta_p} \tau_{prr}^2 = -\eta_p v'$$
$$\tau_{pzz} + \lambda(v\tau'_{pzz} - 2v' \tau_{pzz}) + \alpha \frac{\lambda}{\eta_p} \tau_{pzz}^2 = 2\eta_p v'$$

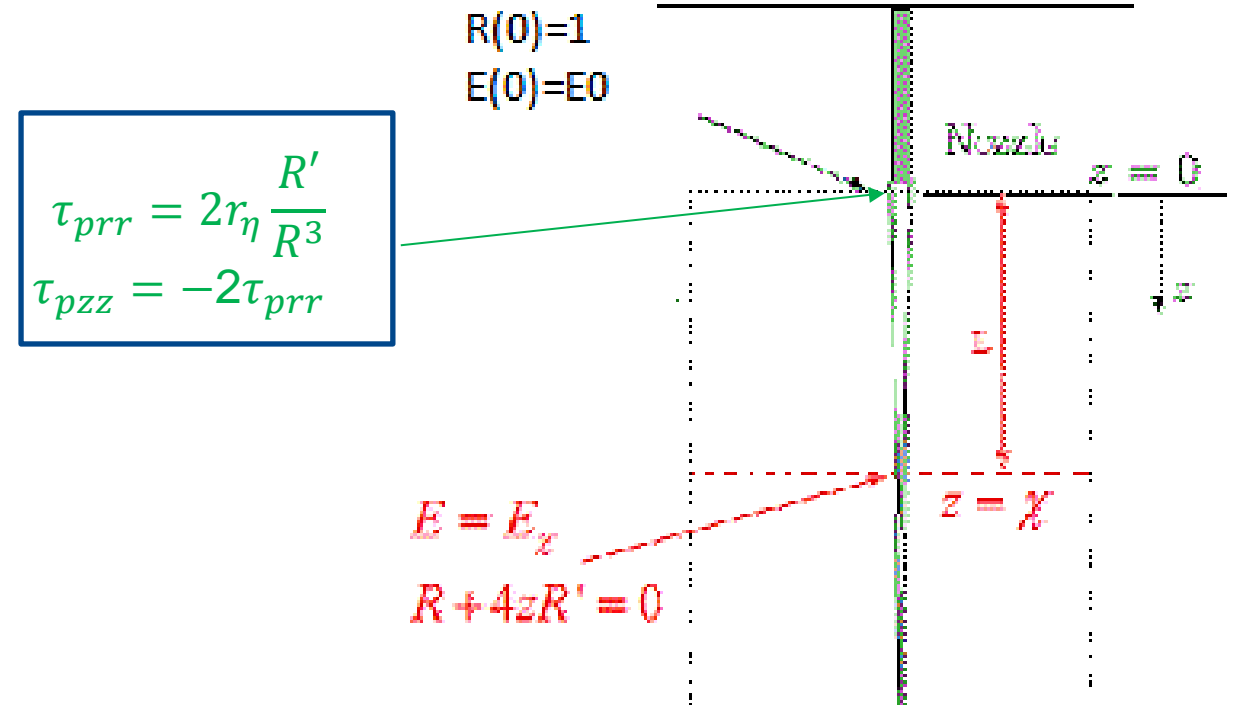
Non-dimensionalised form

$$\tau_{prr} + De(v\tau'_{prr} + v' \tau_{prr}) + \alpha \frac{De}{\eta_p} \tau_{prr}^2 = -r_\eta v'$$
$$\tau_{pzz} + De(v\tau'_{pzz} - 2v' \tau_{pzz}) + \alpha \frac{De}{\eta_p} \tau_{pzz}^2 = 2r_\eta v'$$

Boundary Conditions

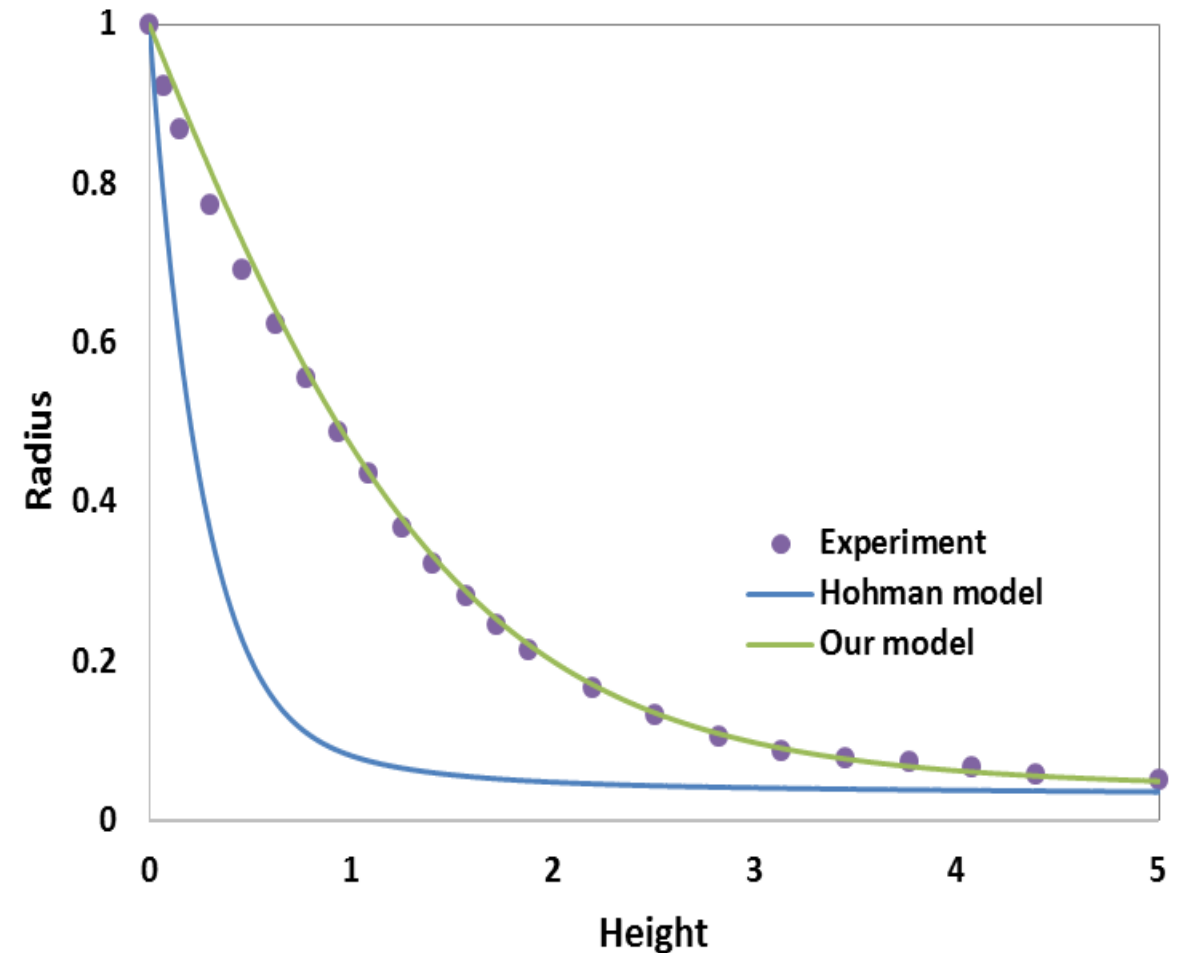
Model is solved for

- 1-D geometry
- R is converted to v using the mass balance equation and then solved
- Mathematics ODE solver is used



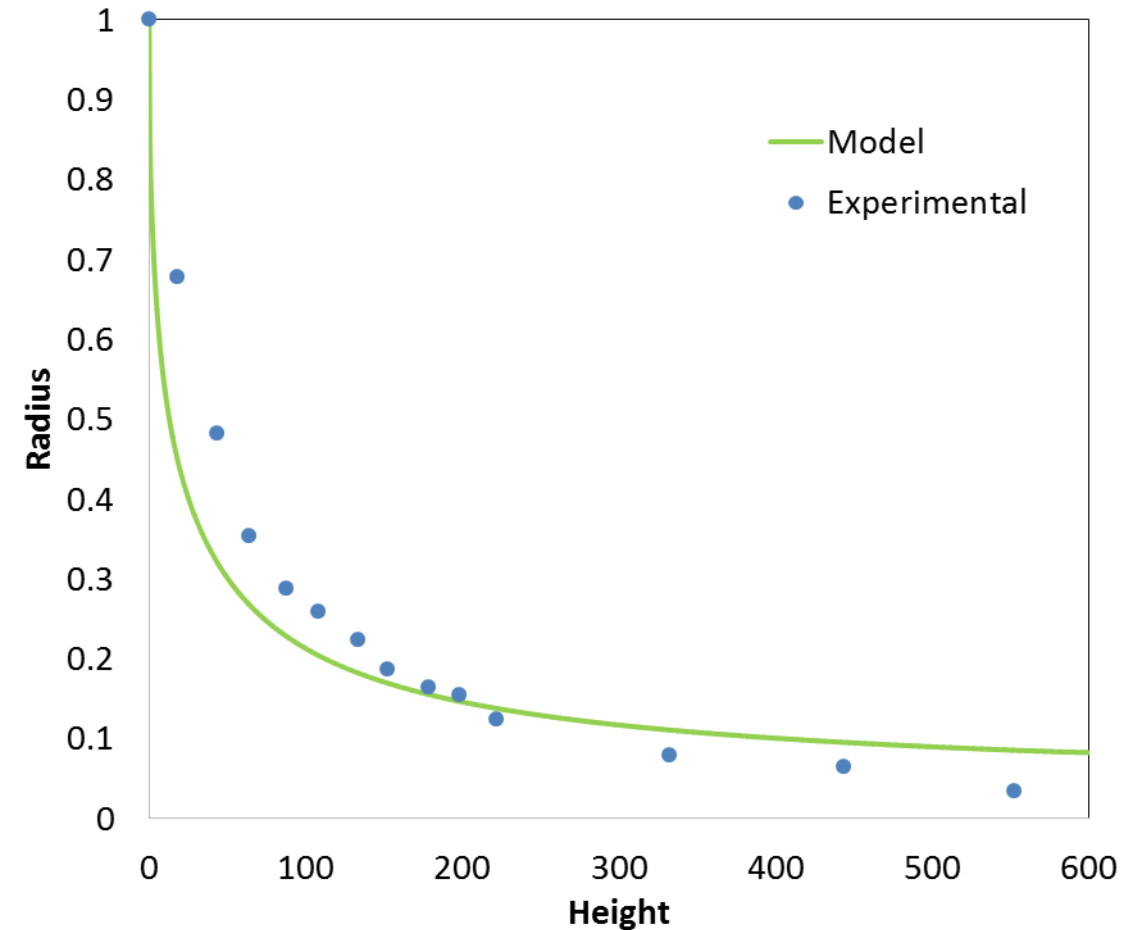
Results

- Experimental data of Hohman *et al.* for a glycerol jet
 - $R_0=0.08$ cm, $L=56$ cm, $Q=1$ mL/min, $E_\infty=5$ kV/cm, $I=170$ nA, kinematic viscosity= 514.9 cm²/s, $K=50.01$ mS/cm
- The parameters of Hohman *et al.*:
 - $X=75$, $B=45.5$, $Re=4.451 \cdot 10^{-3}$,
 $We=1.099 \cdot 10^{-3}$, $Fr=8.755 \cdot 10^{-3}$,
 $Pe=1.8353 \cdot 10^{-4}$, $\varepsilon=0.7311$, $E_\infty=5.914$,
 $K=0.01$ μ S/cm.
- C) All parameters as above with a higher conductivity $K=4.8 \cdot 10^{-6}$ S/m, corresponding to $Pe=3.823 \cdot 10^{-5}$, $\varepsilon=3.173 \cdot 10^{-2}$, and $E_\infty=28.32$.



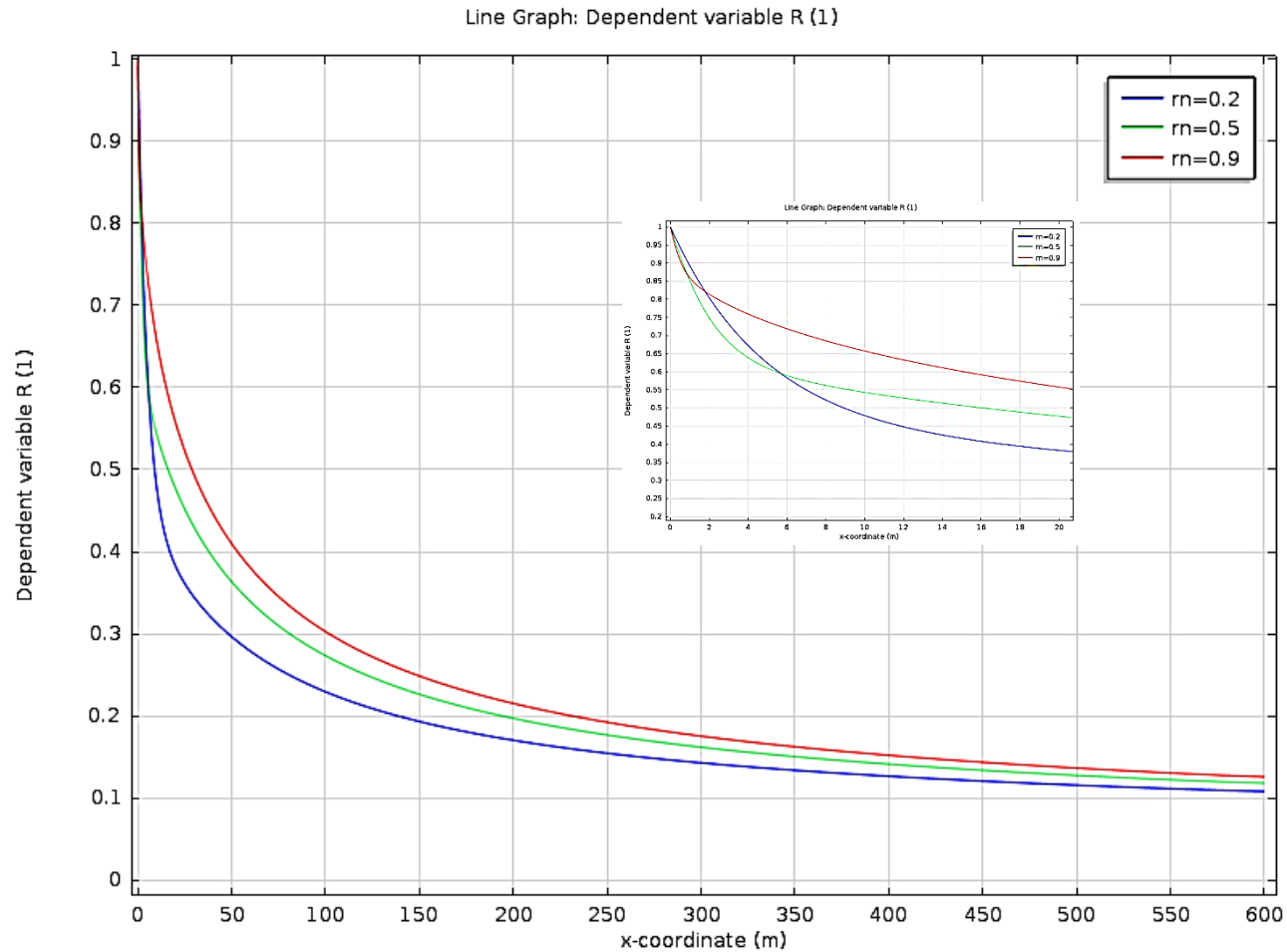
Giesekus model - Validation against Experimental Data

- Experimental data of Doshi et al. for a 4% PEO solution compared against our model.
- Electric field ($E^\infty = 40 \text{ kVm}^{-1}$)
- Nozzle radius ($R_0 = 45 \text{ m}$)
- length of the straight jet ($L = 30 \text{ mm}$).
- The density $\rho = 1.2 \times 10^3 \text{ kgm}^{-3}$
- dielectric constant, $\epsilon / \bar{\epsilon} = 42.7$
- Viscosity, $\eta_0 = 12.5 \text{ P}$;
- surface tension, $\gamma = 76.6 \text{ dyn cm}^{-1}$
- Conductivity, $K = 4.902 \times 10^{-3} \text{ } \Omega^{-1} \text{ m}^{-1}$.
- The solvent viscosity is $\eta_s = 10^{-2} \text{ poise}$ for water
- $I = 0.12 \text{ A}$
- $Q = 10 \text{ } \mu\text{l min}^{-1}$.

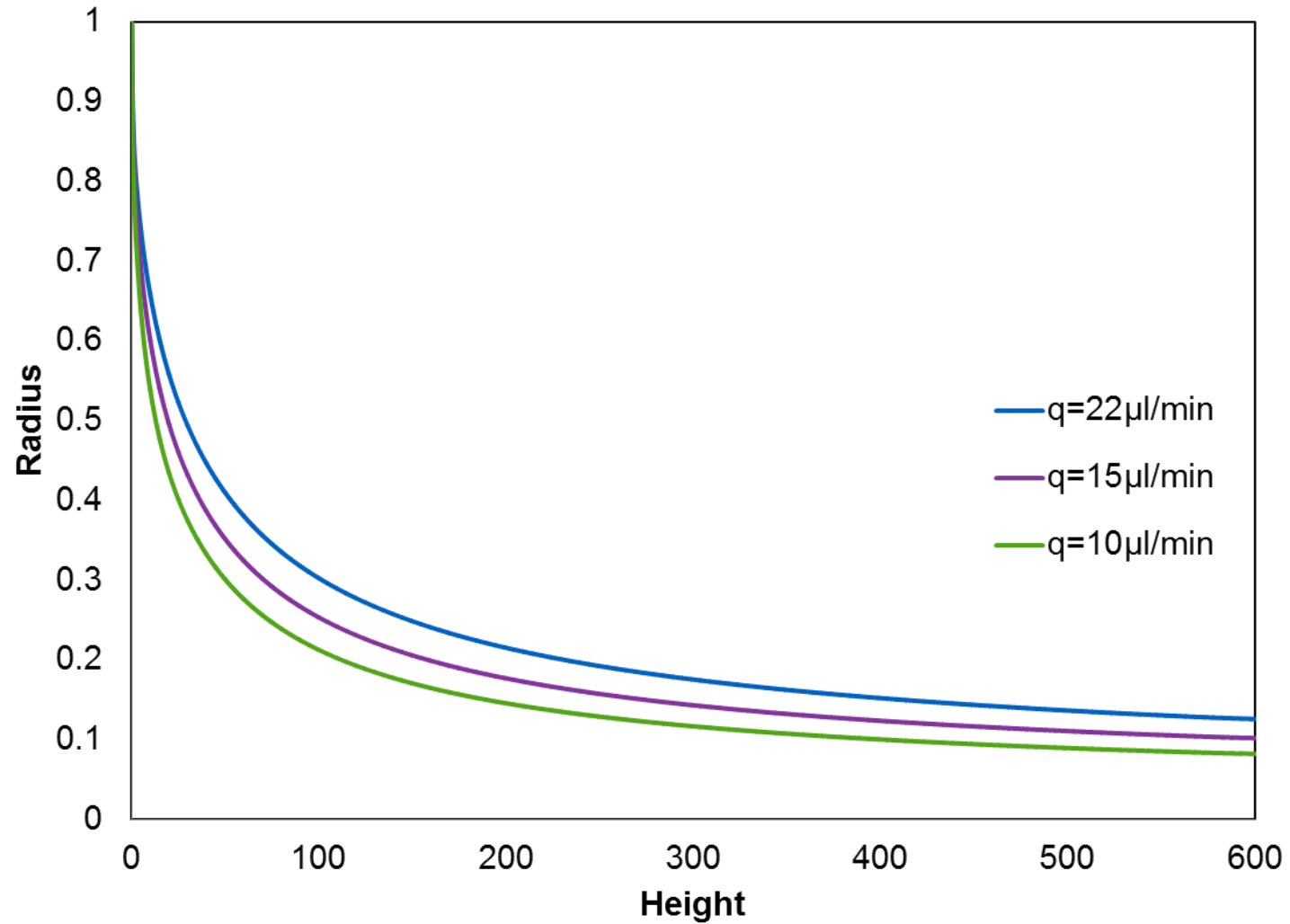


Giesekus Model-Variation with viscosity ratio (r_η)

- Radius vs z



Giesekus Model-Variation with volumetric flow rate (Q)



Conclusion

- A mathematical model was built and validated against experimental data for Newtonian jet and Feng's model for Non-Newtonian jets.
- The model was validated against experimental data for Giesekus model and extended to Oldroyd-B model.
- The model was extended for polymer solution with Non-Newtonian solvent.
- The dependence of the process on different working and material parameters was studied.

THANK YOU