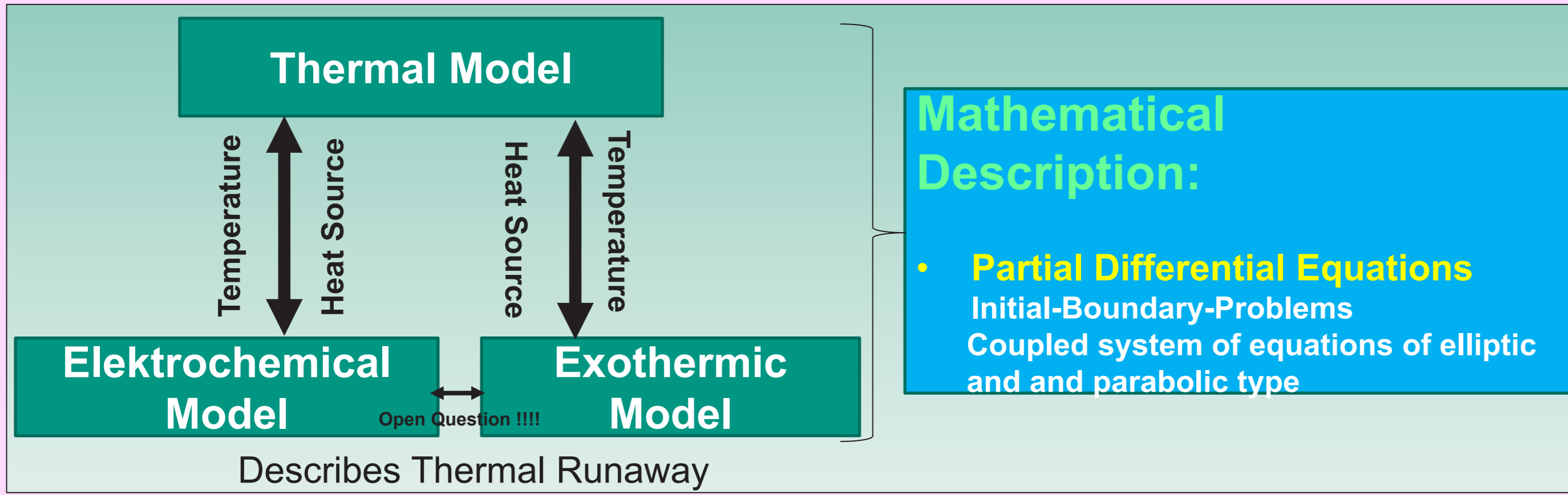


Thermal Modeling of Thermal Runaway of Li-Ion Batteries



Equation-based Thermal Modeling:

Inhomogeneous Heat Transport Equation:

$$\rho c_p \frac{\partial T}{\partial t} = \nabla \cdot (\kappa \nabla T) + Q_{gen}$$

Initial- and Boundary Conditions

$$T(\mathbf{x}, t=0) = T_0(\mathbf{x}), \forall \mathbf{x} \in \bar{\Omega}$$

$$\mathbf{n} \cdot (\kappa \nabla T) = - \underbrace{h(T - T_{env})}_{\text{Convection}} - \underbrace{\epsilon \sigma (T^4 - T_{env}^4)}_{\text{Radiation}}, \forall \mathbf{x} \in \partial \Omega$$

Inhomogeneity: Heat Sources

$$Q_{gen} = Q_{electrochemical} + Q_{exotherm}$$

ρ Density, c_p specific heat capacity, κ heat conduction, Q_{gen} generated heat, \mathbf{n} outwards pointing normal vector, h heat transfer coefficient, T_{env} environmental temperature, ϵ emissivity of cell surface, σ Stefan-Boltzmann-constant ($= 5,670373 \cdot 10^{-8} \text{ W/m}^2 \text{ K}^4$)

Modeling of the Heat Sources:

Electrochemical heat sources from Newman-, Reduced-Order- or ECM-Model

$$Q_{electrochem} = Q_{rev} + Q_{irrev}$$

Thermodynamic Reversible Heat: $Q_{rev} = I \cdot T \cdot \frac{\partial U_{eq}}{\partial T}$ Thermodynamic Irreversible Heat: $Q_{irrev} = (U_{eq} - U) \cdot I$

U cell voltage, I current, U_{eq} open circuit voltage (OCV)

Exothermic Heat Source from Combustion-Model/Solid-Fuel-Modell

$$Q_{exotherm} = Q_{sei} + Q_{pe} + Q_{ne} + Q_{ele}$$

- $T > T_1$: Decomposition of the Solid Electrolyte Interface in a exothermic reaction $\Rightarrow Q_{SEI}$
- $T > T_2$: Exothermic reaction between the intercalated Lithium-ions in the negative electrode and the electrolyte \Rightarrow reduction of the electrolyte at the negative electrode $\Rightarrow Q_{NE}$
- $T > T_3$: Exothermic reaction between active particles of the positive electrode and the electrolyte \Rightarrow rapid generation of oxygen $\Rightarrow Q_{PE}$
- $T > T_4$: Exothermic decomposition of the electrolyte $\Rightarrow Q_{ELE}$

Combustion-Model/Solid-Fuel-Model: General Formulation

$$\frac{\partial c_i}{\partial t} = \nabla \cdot (d_i \nabla c_i) - R_i, i \in \{sei, pe, ne, ele\}$$

$$R_i(T, c_i) = k_i(T) \cdot f_i(c_i)$$

$$k_i(T) = A_i \cdot \exp\left(-\frac{E_{a,i}}{RT}\right)$$

$$f_i(c_i) = c_i^{m_i} (1 - c_i)^{n_i} (-\ln(1 - c_i))^{p_i}$$

$$Q_i = q_i \cdot R_i$$

c_i Dimensionless concentration of Lithium ions in the i -th reactant, m_i, n_i, p_i reaction rates, d_i Diffusion coefficient, A_i Frequency factor, $E_{a,i}$ Activation energy, R General gas constant, i.e. $R = 8.314462 \text{ J/mol K}$

+ Initial- and Boundary-Conditions

Simplification: Constant Fuel Model

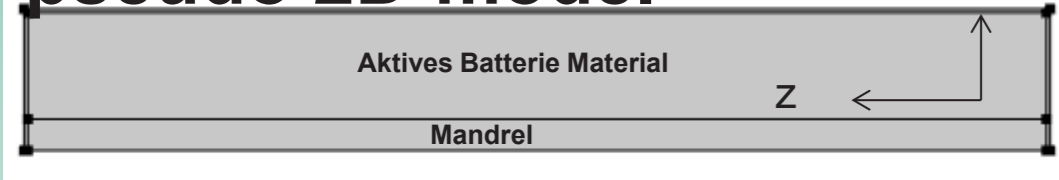
$$\frac{\partial c_i}{\partial t} = 0$$

$$c_i = const = c_{i,0}$$

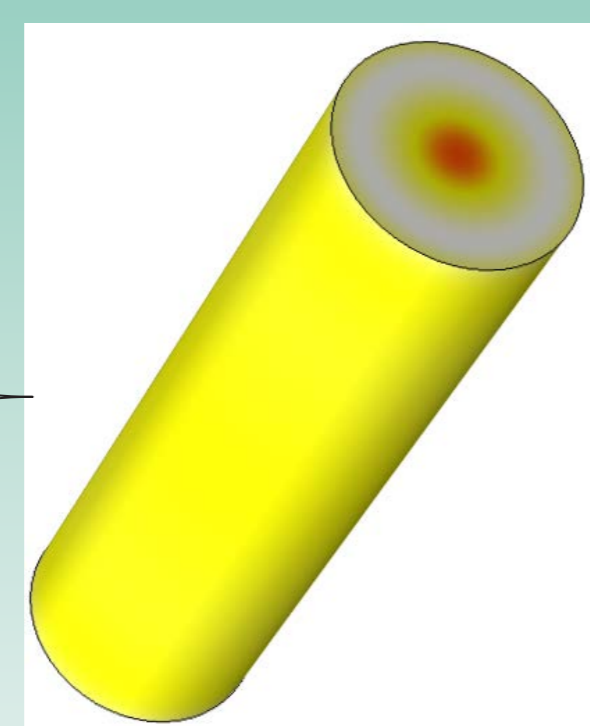
$$f(c_i) = const = \tilde{c}_i$$

Simulation of a Single 18650 Cell with a LiCoO₂ Cathode in Comsol Multiphysics:

Geometry: Axial-symmetric pseudo 2D-model



Meshing: Adaptive Triangulation, Quadratic Basis-Functions

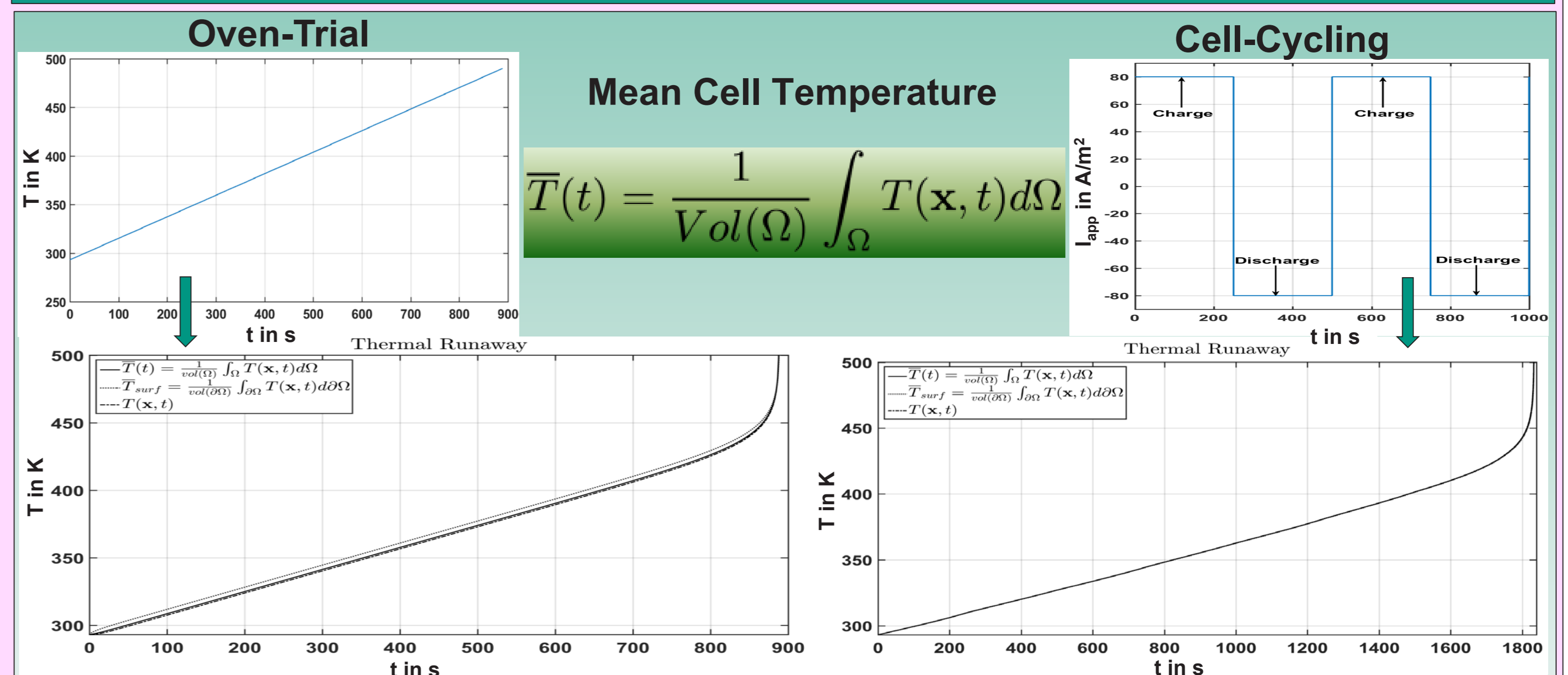


- Exothermic Model: Constant Fuel Model
- Time Integration: BDF 15
- Spatial Discretisation: FEM
- Oven-Trial
- Cell-Cycling

Simulation Results:

- Temperature field: $T(\mathbf{x}, t)$
- Mean cell temperature: $\bar{T}(t)$
- Temperaturprofile
-

Simulation Results:

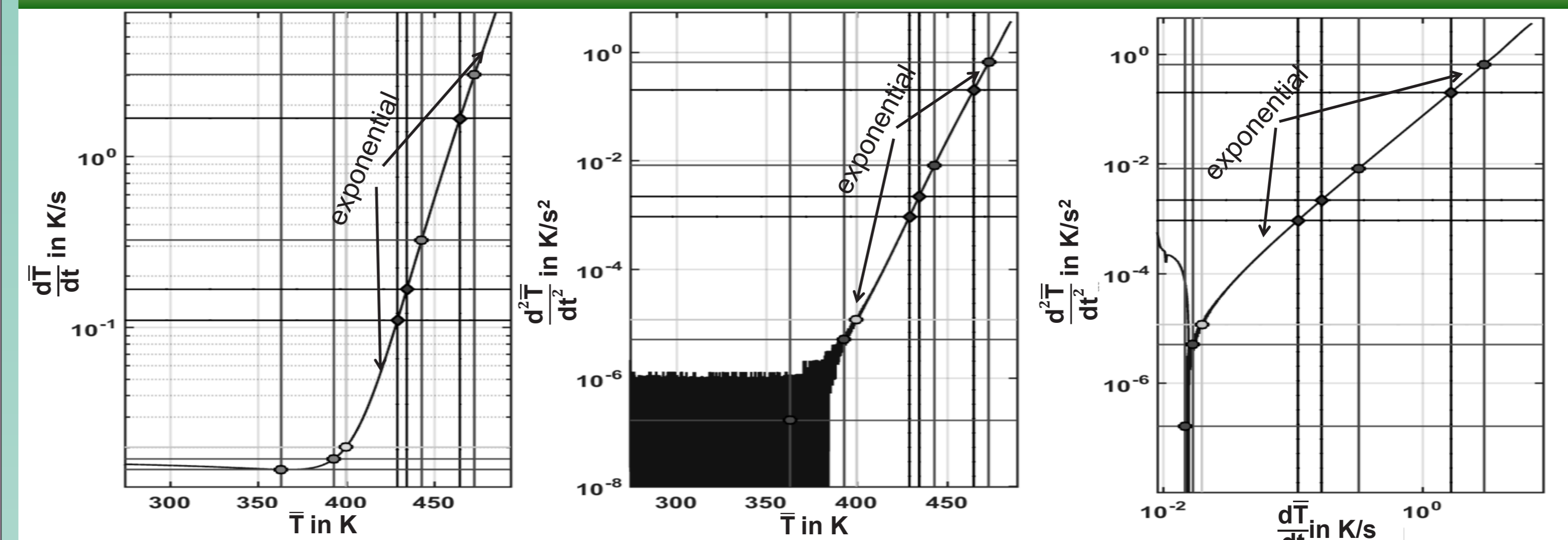


Classification of Thermal Runaway

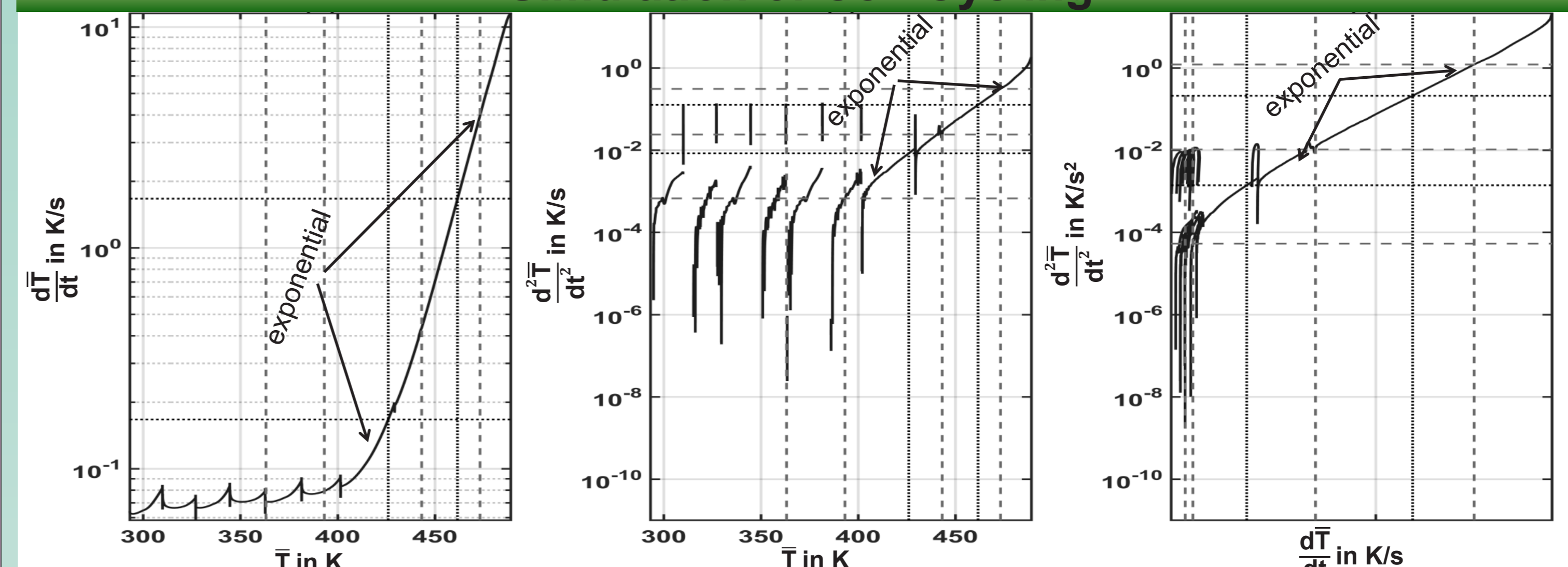
Phase Space

$$\left(\bar{T}, \frac{d\bar{T}}{dt}, \frac{d^2\bar{T}}{dt^2} \right) \subset \Omega_3 \in \mathbb{R}^3$$

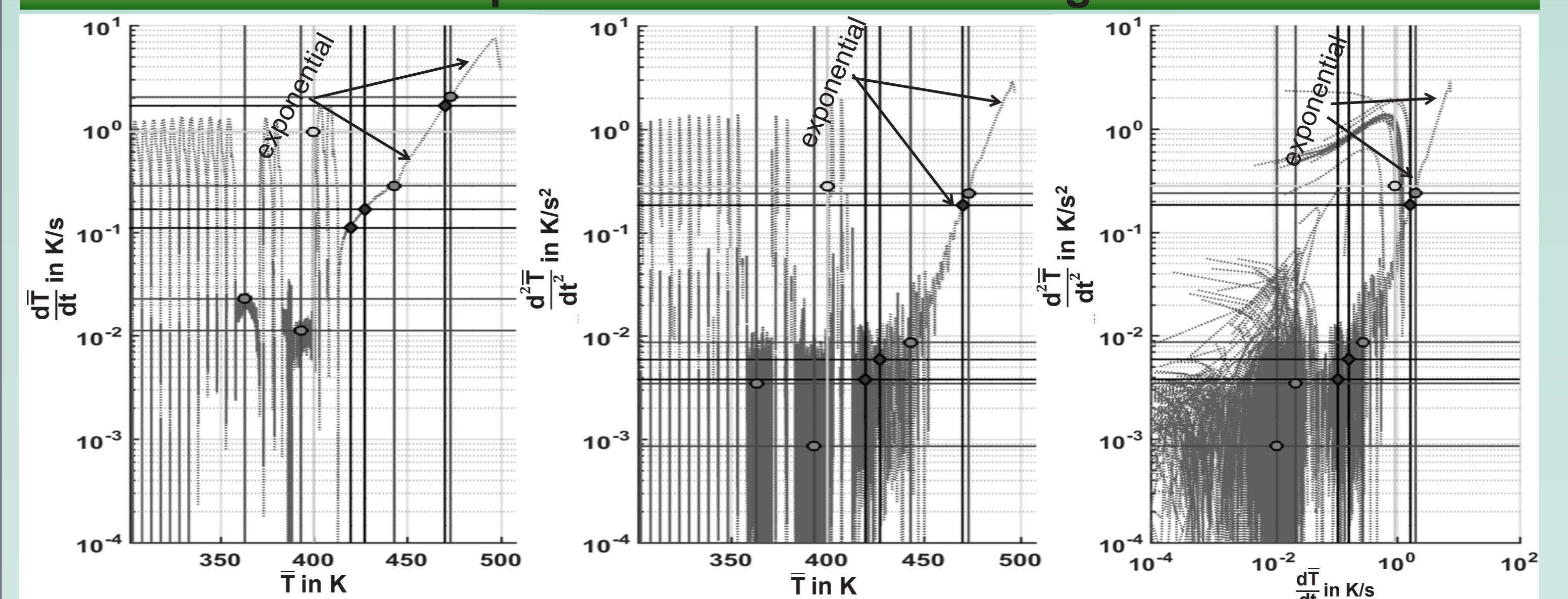
Simulation of a Oven Trial



Simulation of Cell-Cycling



Heat-Wait-Seek Experiment in an Accelerating Rate Calorimeter



Classification:

