



Finite Element Modeling of Coupled Heat and Mass Transfer of a Single Maize Kernel Based on Water Potential Using COMSOL Multiphysics Simulation



Authors:

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**Main research area of our Institute is
grain drying since the 1980's.**

Introduction



Testing of grain dryers



Thermographic image
of the dryer



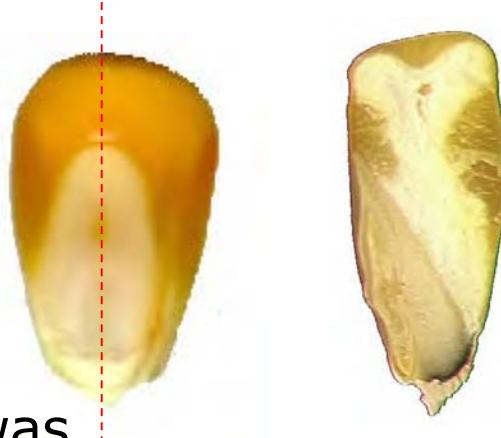
**Experimental convective
drying tunnel**



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Besides experimental research drying modeling of a single kernel was initiated.



For example, the **mass diffusion** relationship was determined for different maize hybrids:

$$D = e^{a+bX+cT^{-1}}$$

where: D = moisture diffusion coefficient;

X = kernel average moisture content (dry basis);

T = average temperature of kernels;

a, b, c = constants.

(These constants for the Pioneer 3780 hybrid were found: $a = -3.1411$; $b = 3.2159$; $c = -6696.6$)



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Based on the measurements mathematical modeling studies of drying were carried out using Finite Element method:

$$\rho \cdot c \frac{\partial T}{\partial t} = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) + L \cdot \rho \frac{\partial X}{\partial t}$$

for heat transfer

$$\frac{\partial X}{\partial t} = D \left(\frac{\partial^2 X}{\partial x^2} + \frac{\partial^2 X}{\partial y^2} \right)$$

for mass transfer

where: X is moisture content d.b. [kg/kg];
 ρ is density [kg/m^3];
 T is temperature [K];
 K is thermal conductivity [W/mK];
 L is latent heat of vaporisation
of water [J/kg].

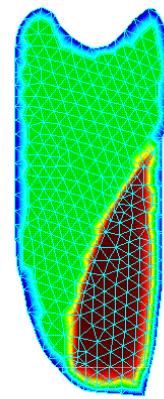
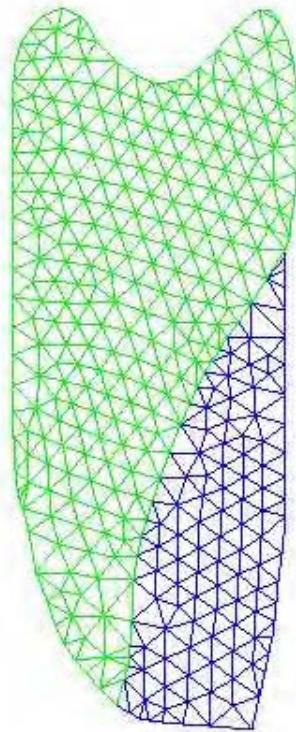
D is diffusion coefficient [m^2/s];
 c is specific heat [J/kgK];
 t is time [s];
 x, y are directions;



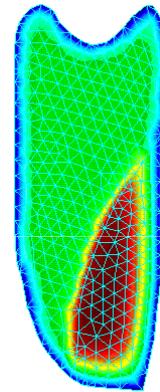
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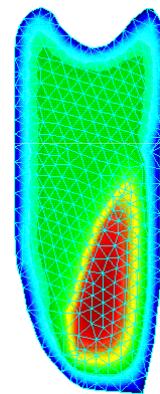
FE modelling with **COSMOS 1.71**



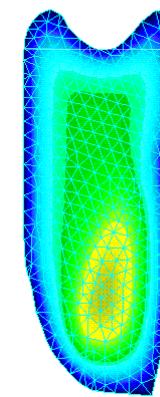
5 min



35 min



50 min



85 min of drying

Mass transfer

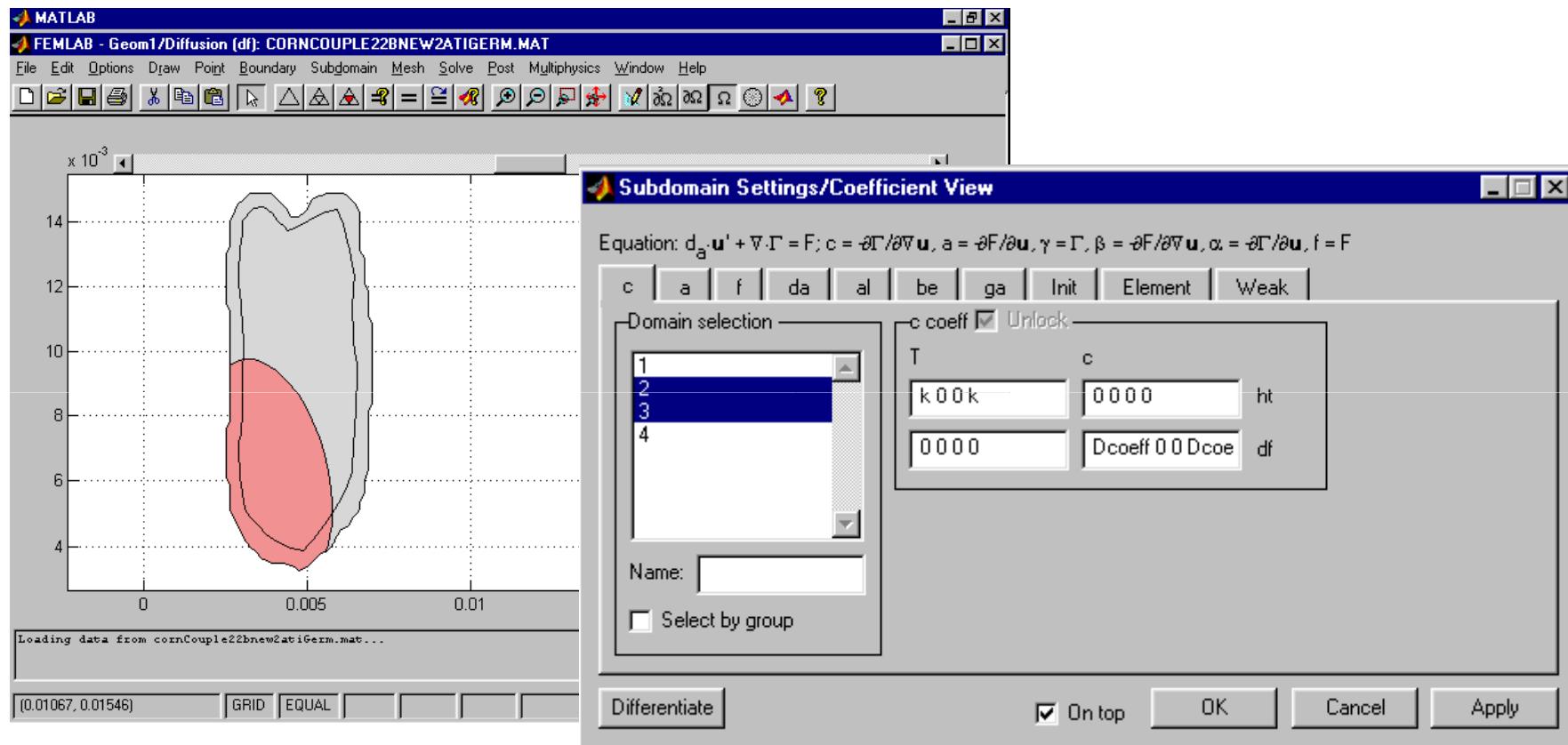


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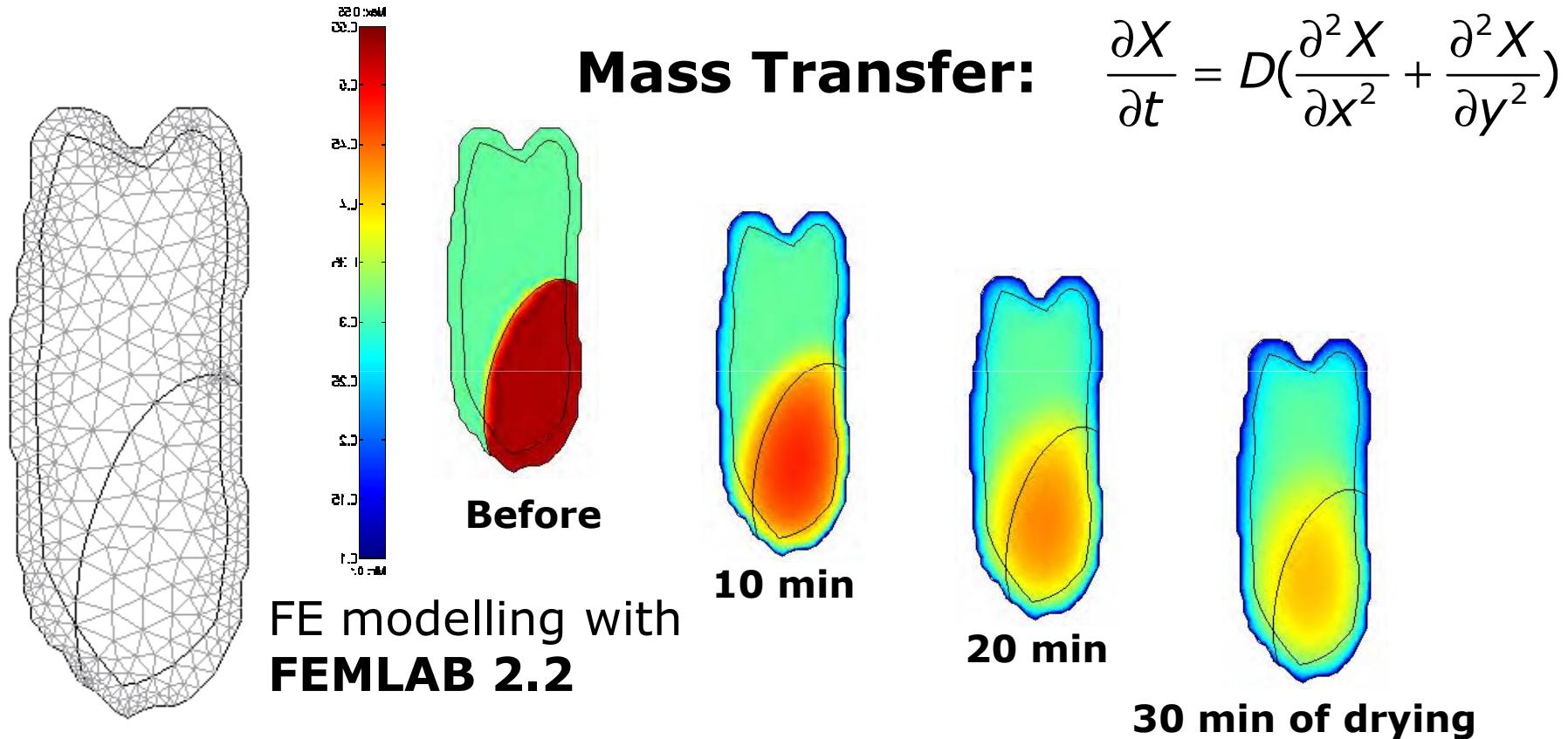
COMSOL MULTIPHYSICS simulation (FEMLAB 2.2 package)



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Heat Transfer: $\rho \cdot c \frac{\partial T}{\partial t} = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) + L \cdot \rho \frac{\partial X}{\partial t}$



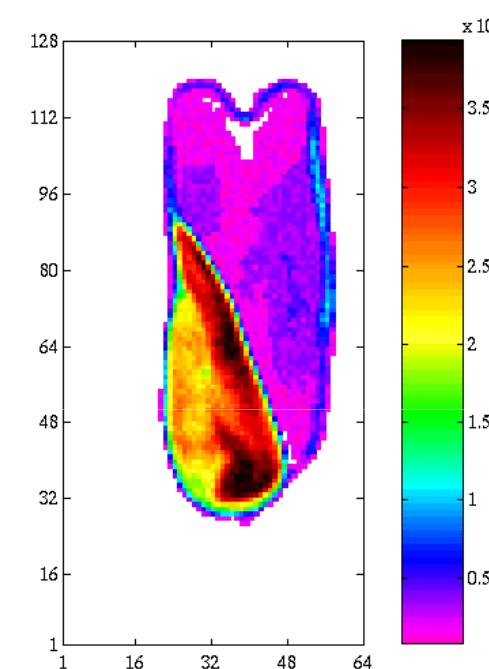
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**Magnetic resonance imaging (MRI)
studies were carried out to evaluate the
accuracy of the FE models.**



NMR magnet at BRUKER GMBH



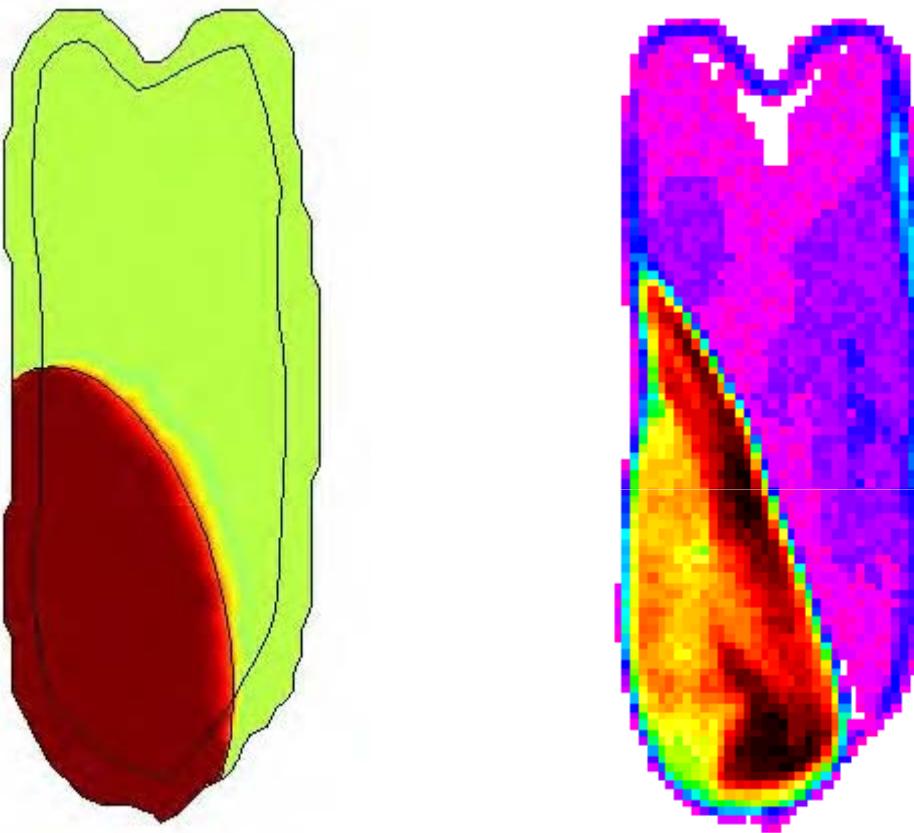
**MRI image of a corn
kernel before drying**



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MRI measurement:



FEMLAB model: the moisture content changes inside a single kernel during drying.

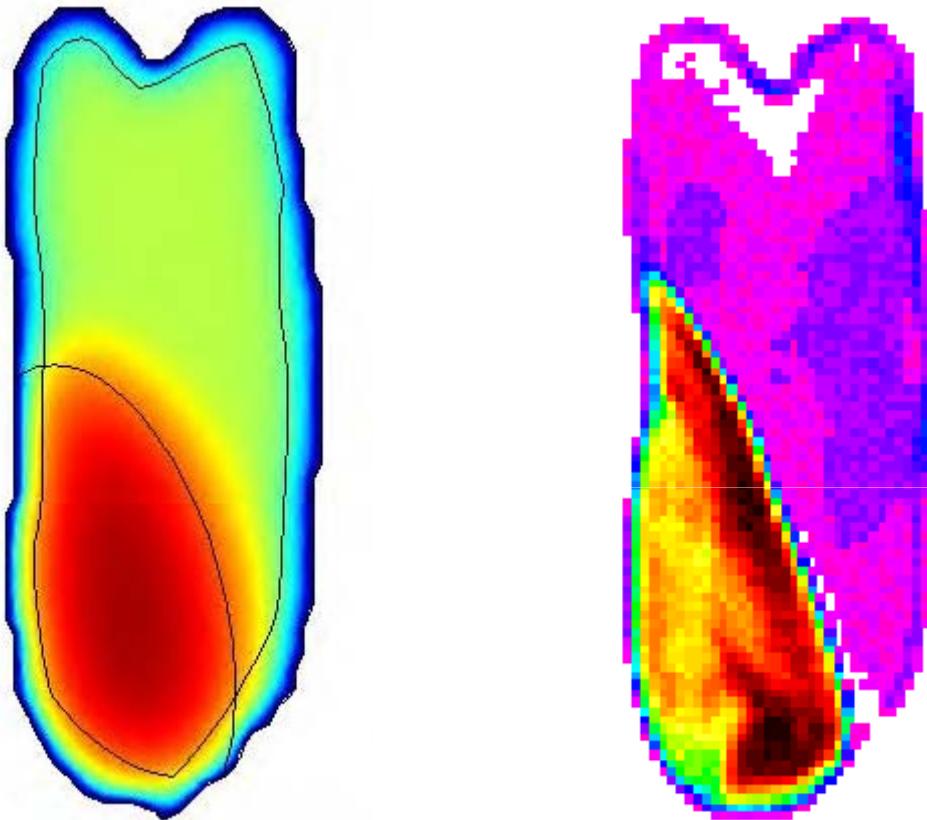
- the model is based on the **m.c. gradients**



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MRI measurement:



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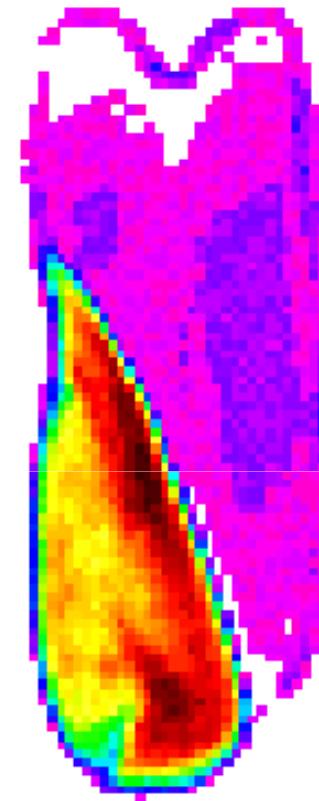
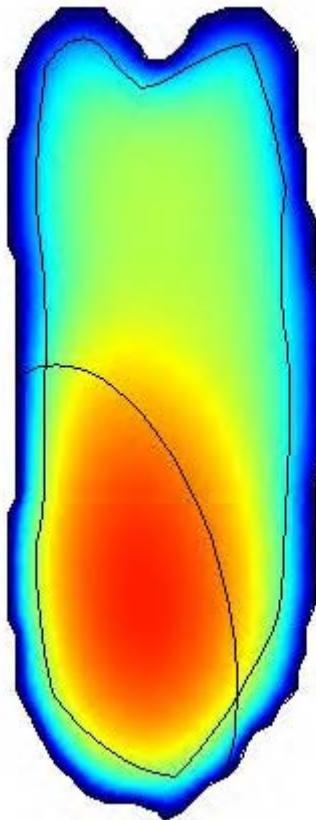
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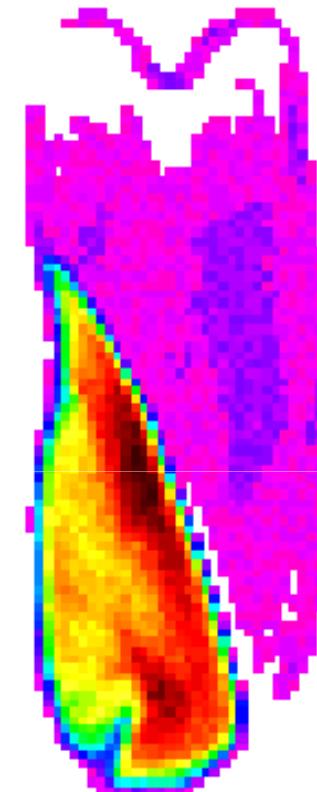
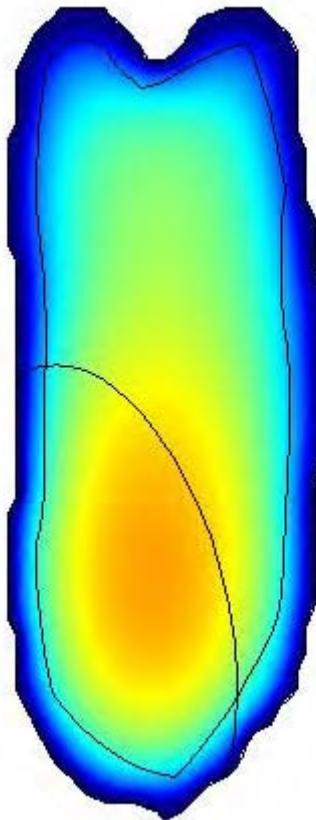
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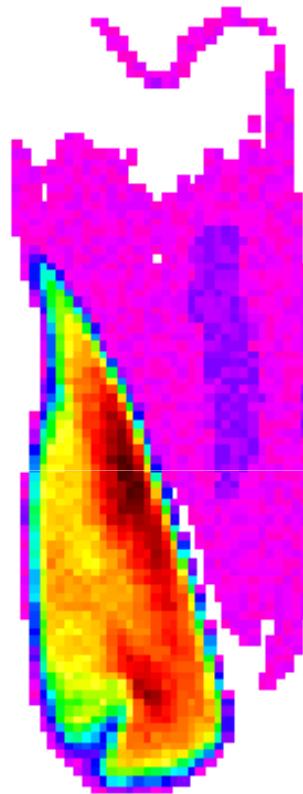
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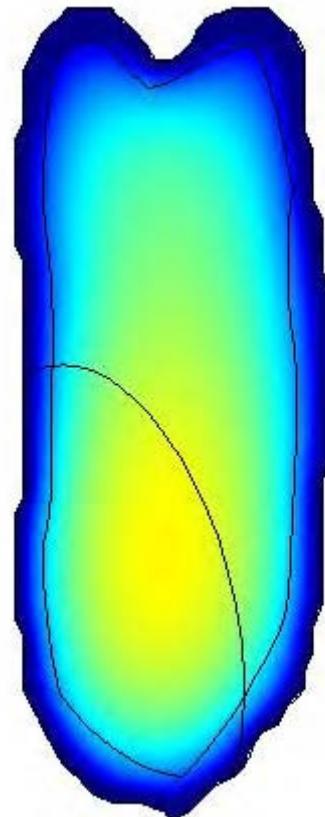
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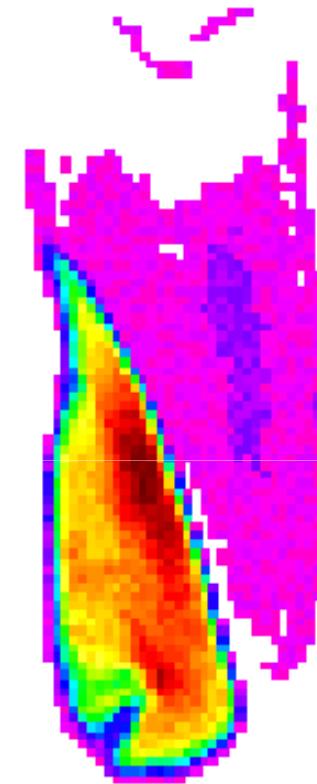
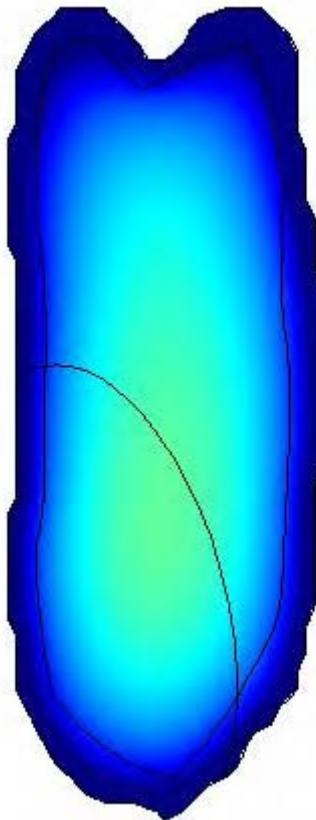
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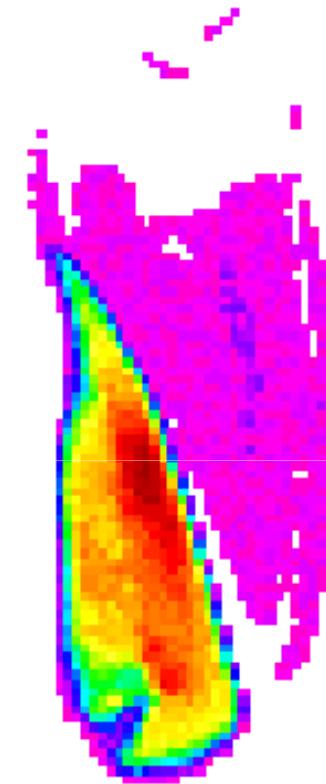
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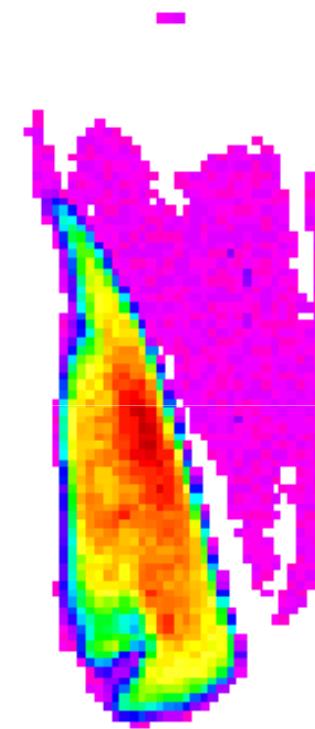
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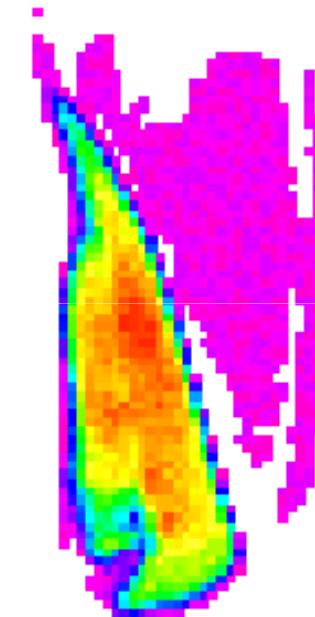
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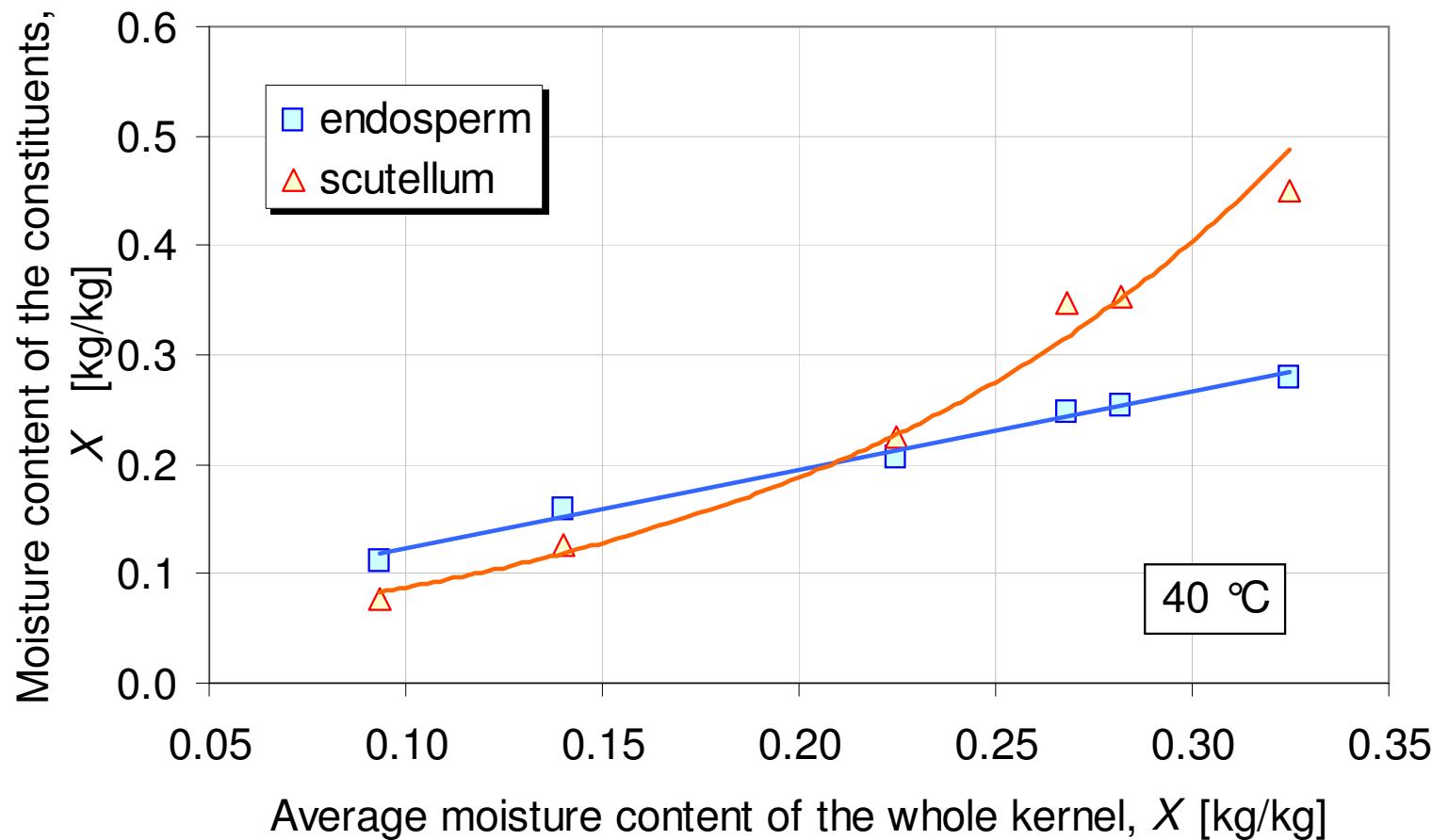
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Moisture content of the particles vs. whole maize kernels (Florence)



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Considering capillary (water) potential

The modified **Luikov's model** of mass transport,

$$\frac{\partial X}{\partial \tau} = \operatorname{div} D \cdot \operatorname{grad} X$$

where: X is moisture content;
 τ is time;
 D is mass diffusion coefficient.

can be **rewritten**:

$$\frac{\partial X}{\partial \Psi} \frac{\partial \Psi}{\partial \tau} = \frac{\partial}{\partial x} \left[D \frac{\partial X}{\partial \Psi} \cdot \frac{\partial \Psi}{\partial x} \right] + \frac{\partial}{\partial y} \left[D \frac{\partial X}{\partial \Psi} \cdot \frac{\partial \Psi}{\partial y} \right] + \frac{\partial}{\partial z} \left[D \frac{\partial X}{\partial \Psi} \cdot \frac{\partial \Psi}{\partial z} \right]$$

and thus the equation **gives**:

$$\frac{\partial X}{\partial \Psi} \frac{\partial \Psi}{\partial \tau} = \operatorname{div} K \cdot \operatorname{grad} \psi$$

where: Ψ is capillary (water) potential;
 K is hydraulic conductivity ($K = D \cdot \partial X / \partial Y$).



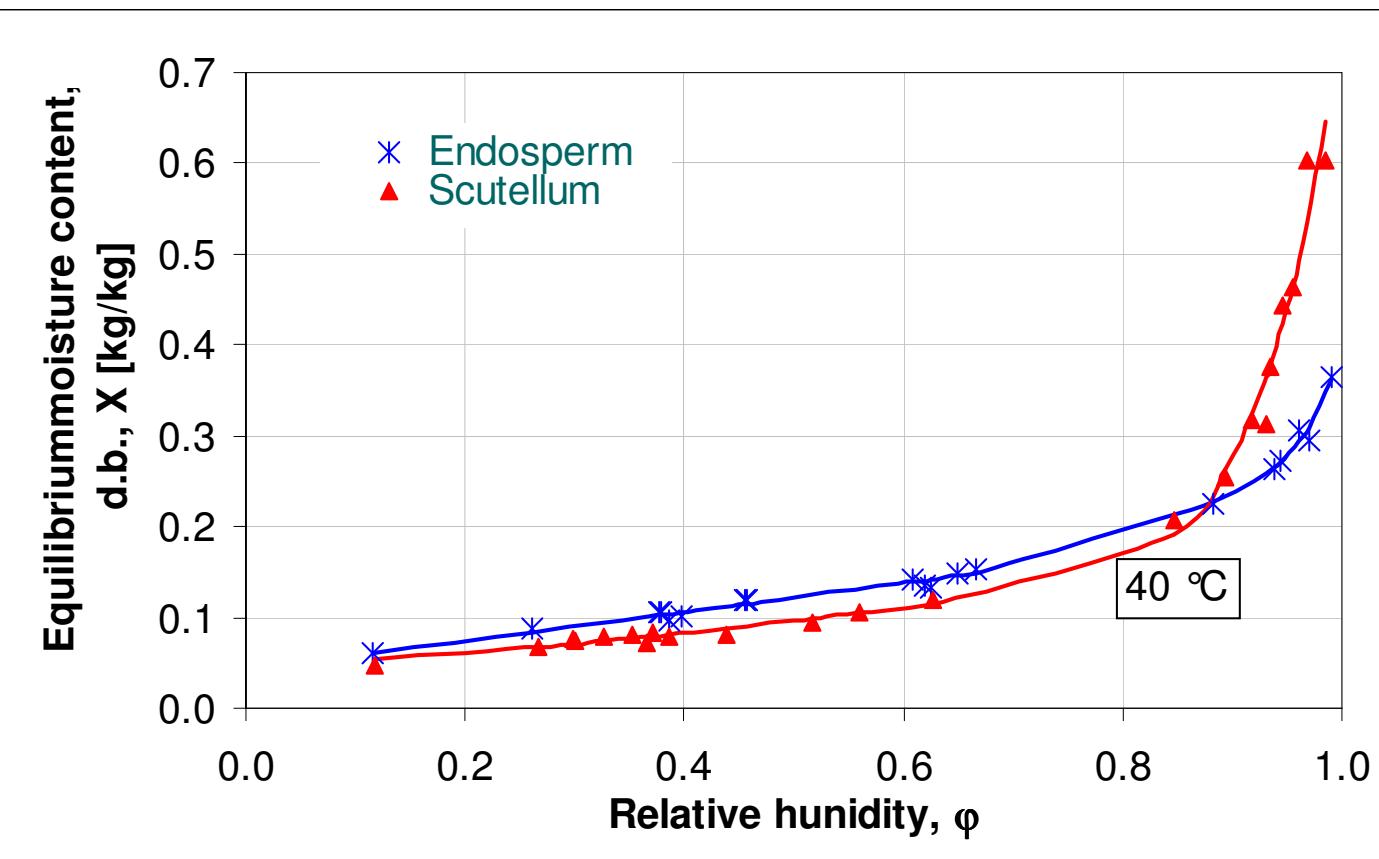
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Desorption curves of maize kernel's particles



ROTRONIC water
activity meter



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Water potential curves of maize particles as a function of moisture content

$$[\Psi]_X = \frac{R_U \cdot T}{m_v} \ln \varphi$$

where:

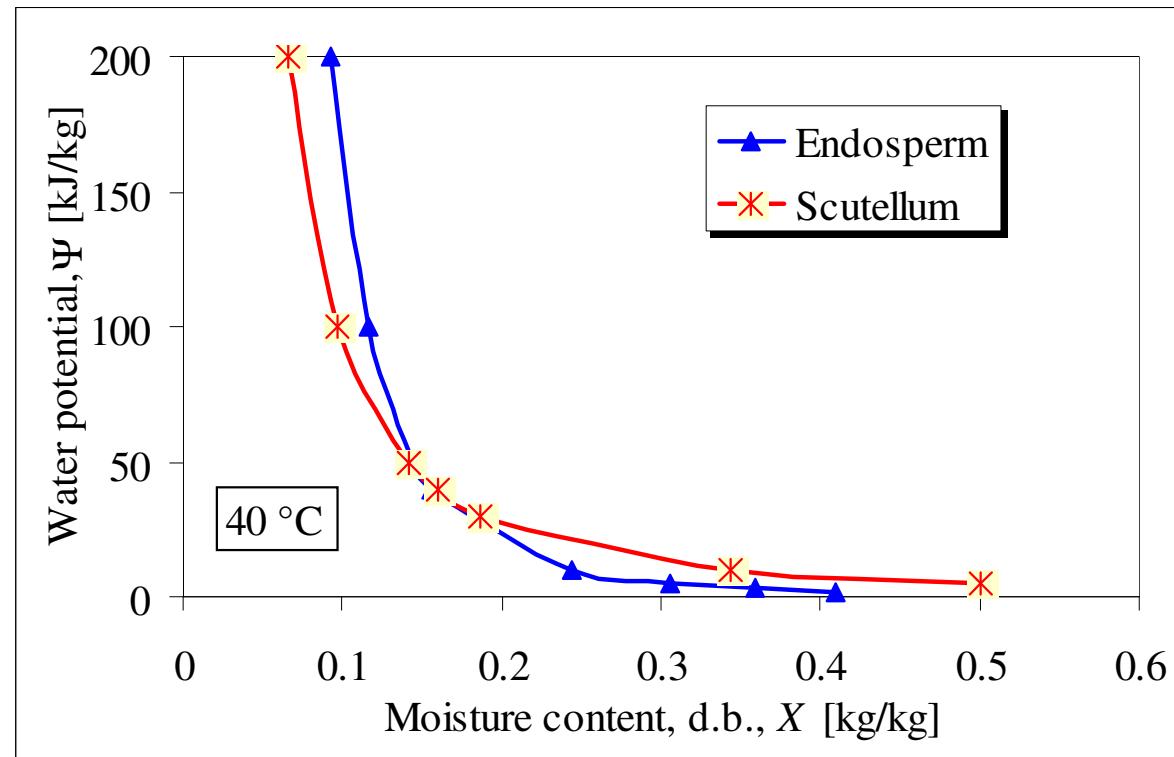
φ is the relative humidity of the air (decimal);

R_U is the universal gas constant;

m_v is the molecular weight of vapour;

T is the absolute temperature;

X is moisture content, d.b.



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Boundary conditions

Neumann type:

$$\underline{n} \cdot (c \nabla u) + qu = qu_\infty$$

where:

u is stands for the water potential (Ψ);

\underline{n} is the normal vector.

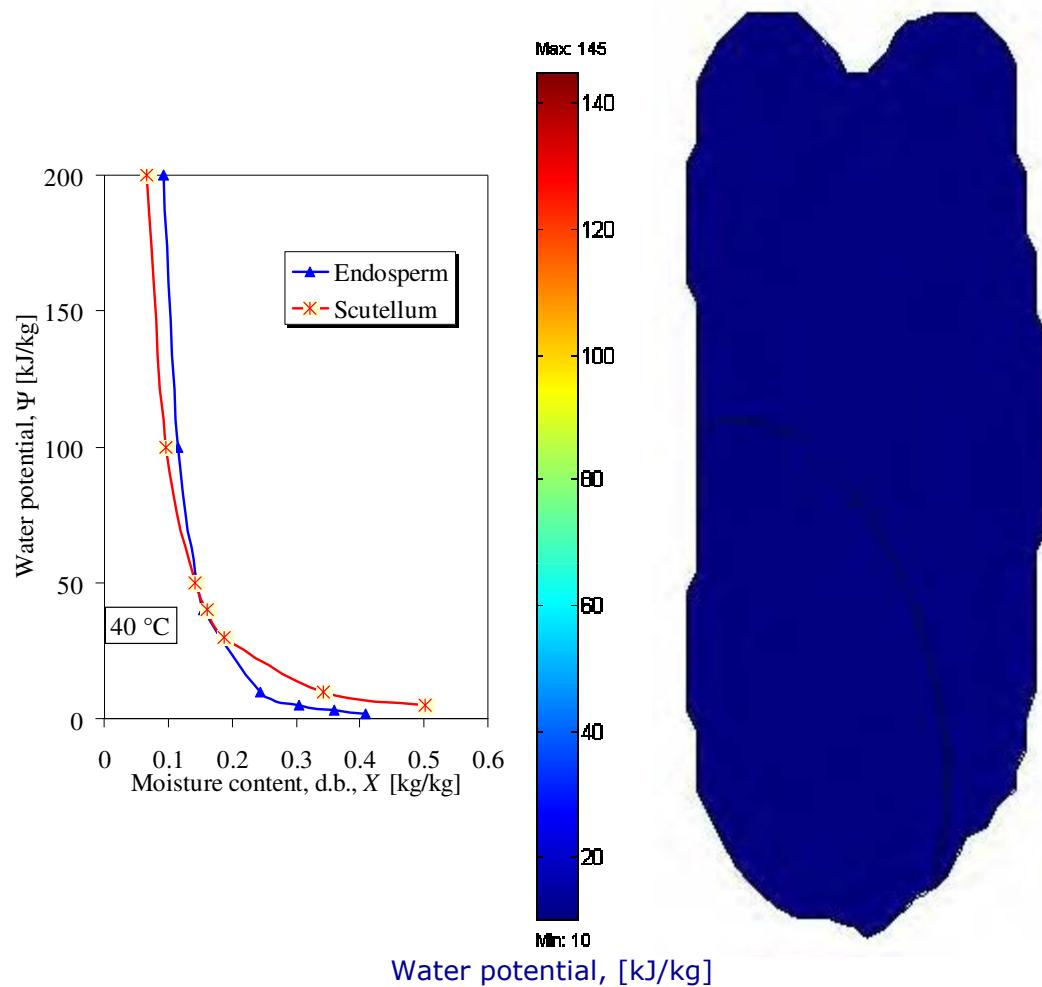
$$d_a = \frac{\partial X}{\partial \psi}$$



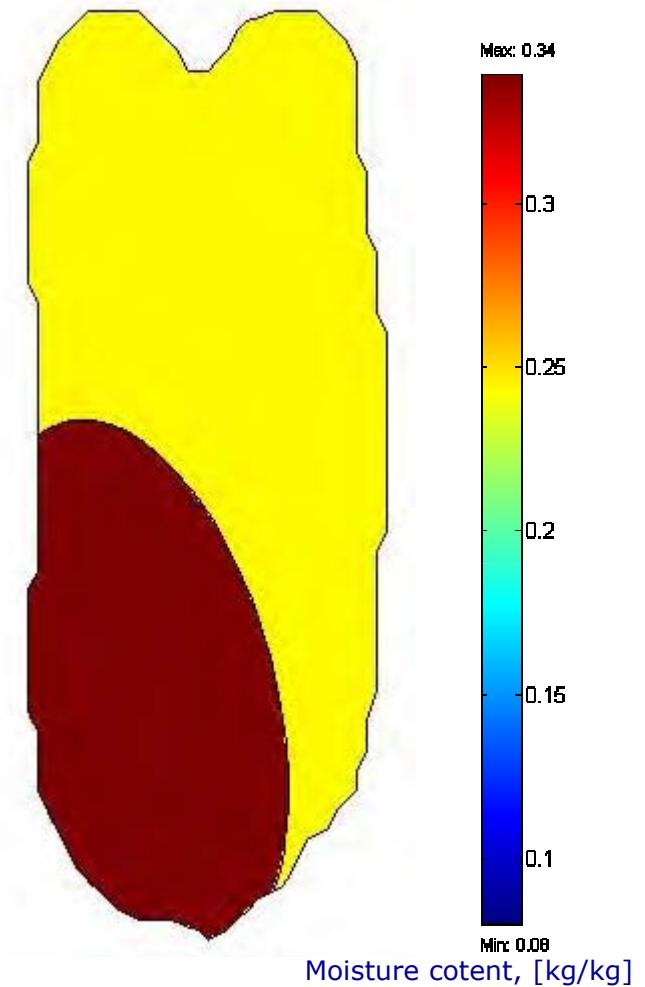
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Modelled Ψ changes



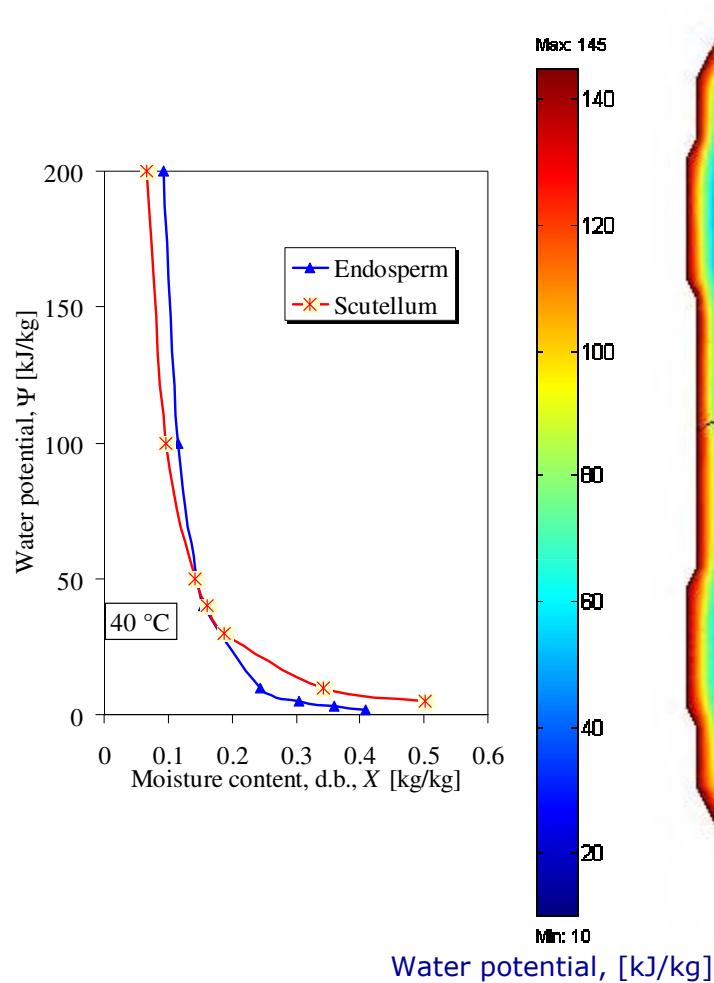
X changes based on grad Ψ



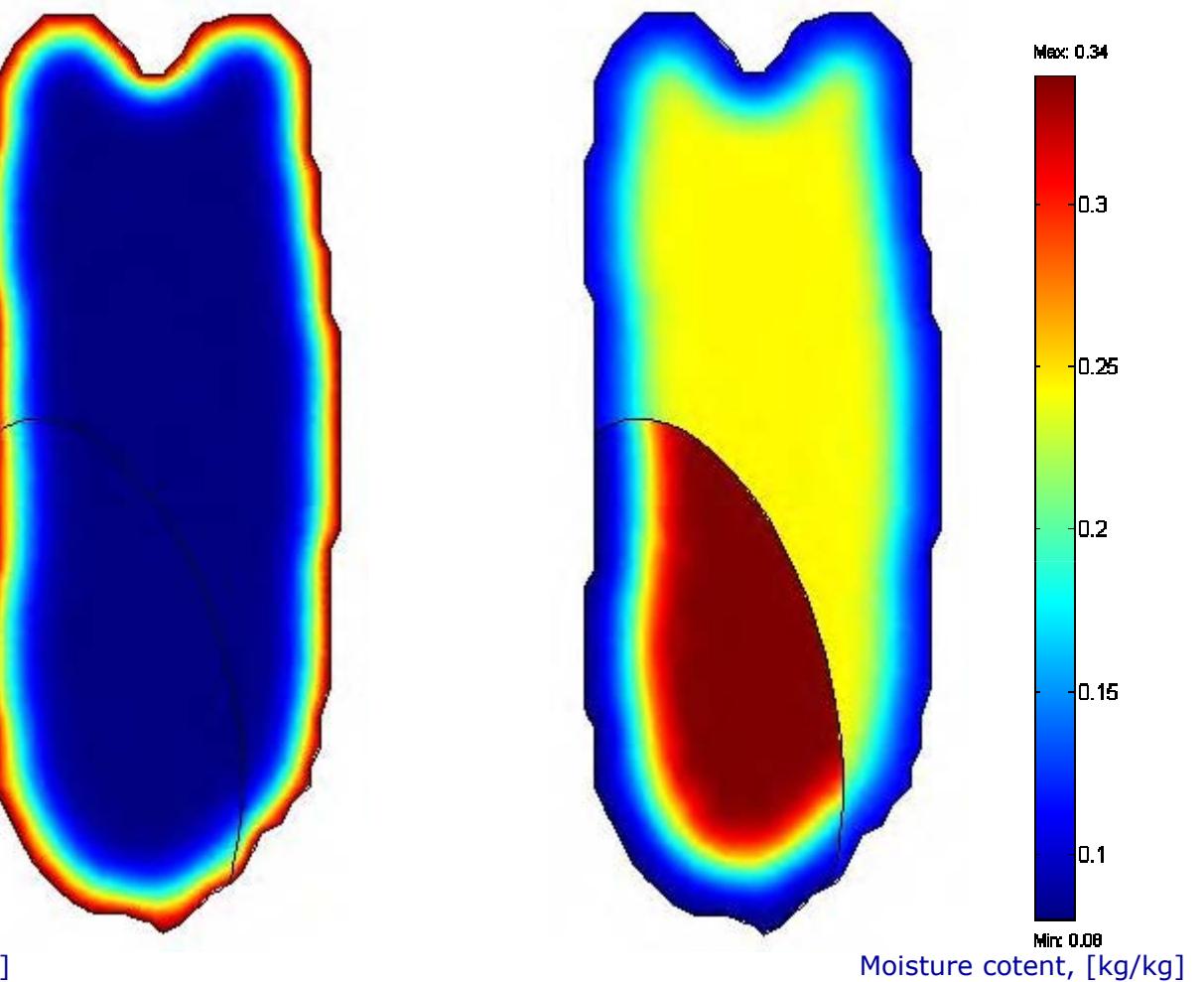
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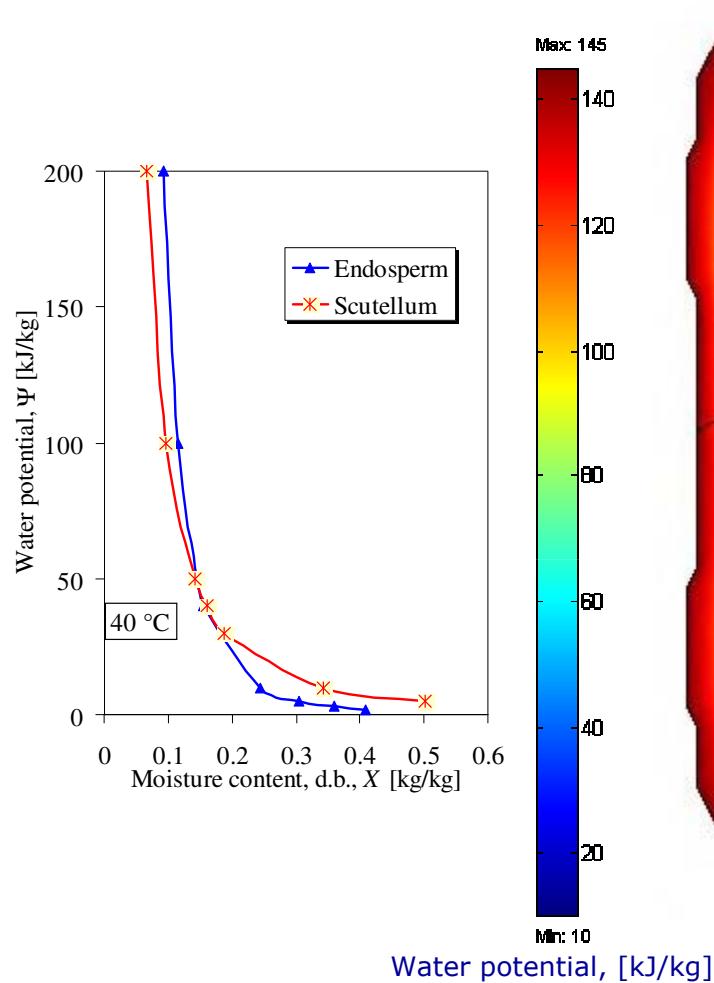
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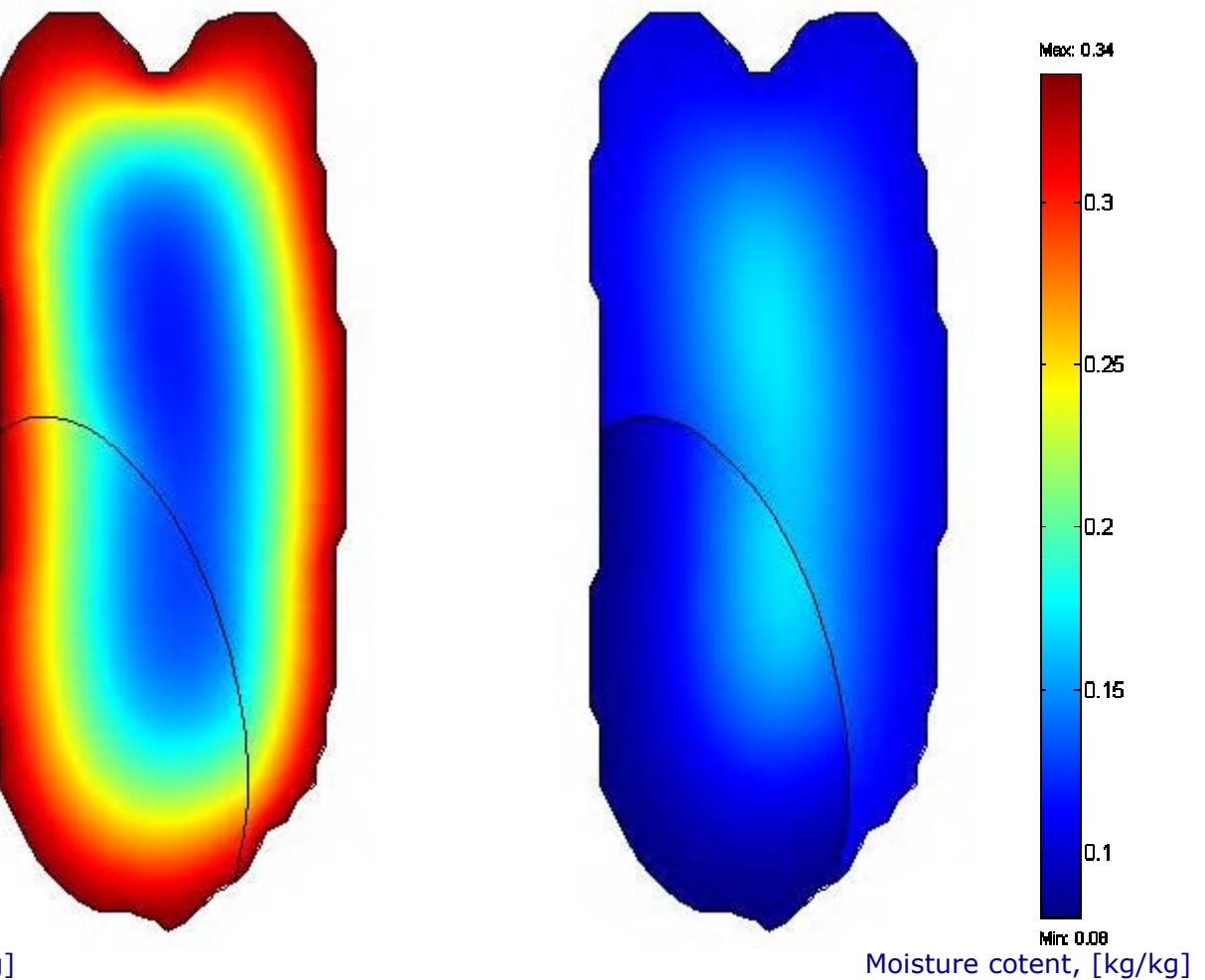
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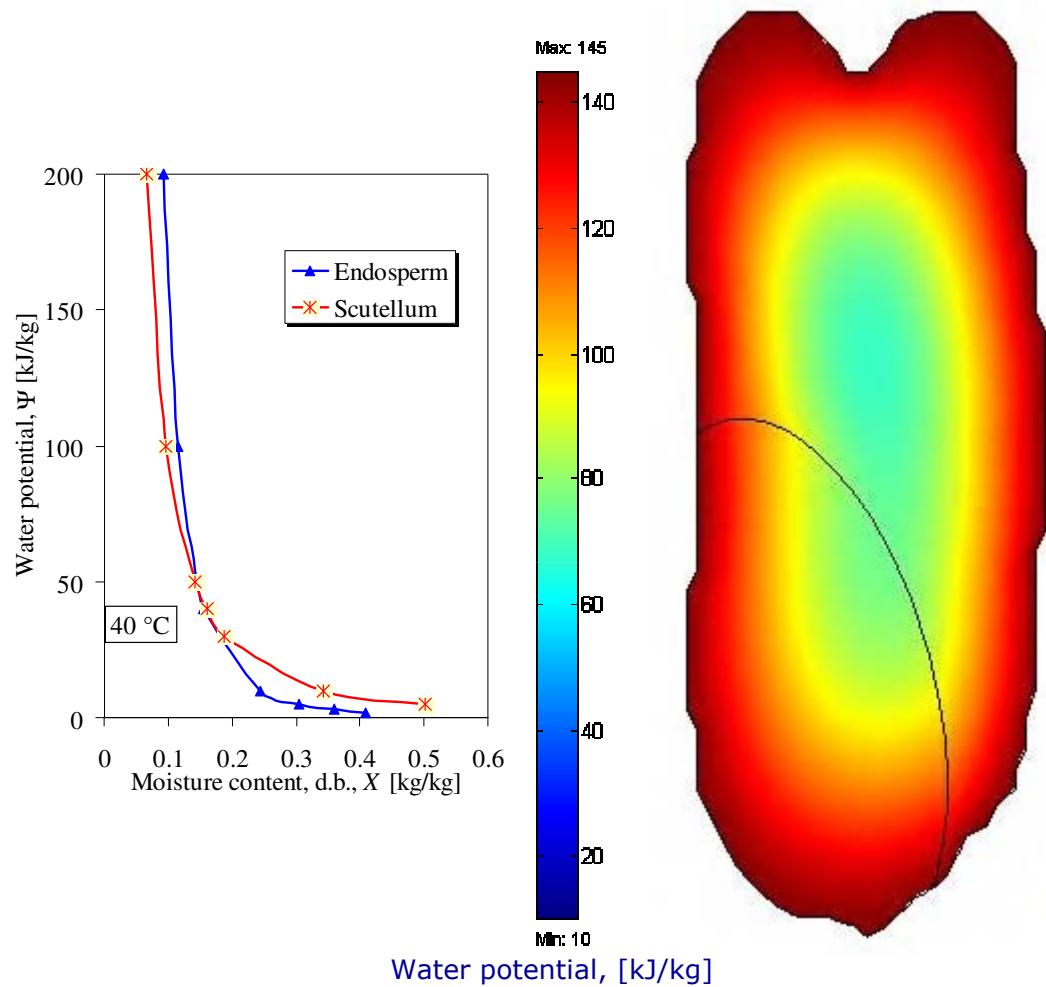
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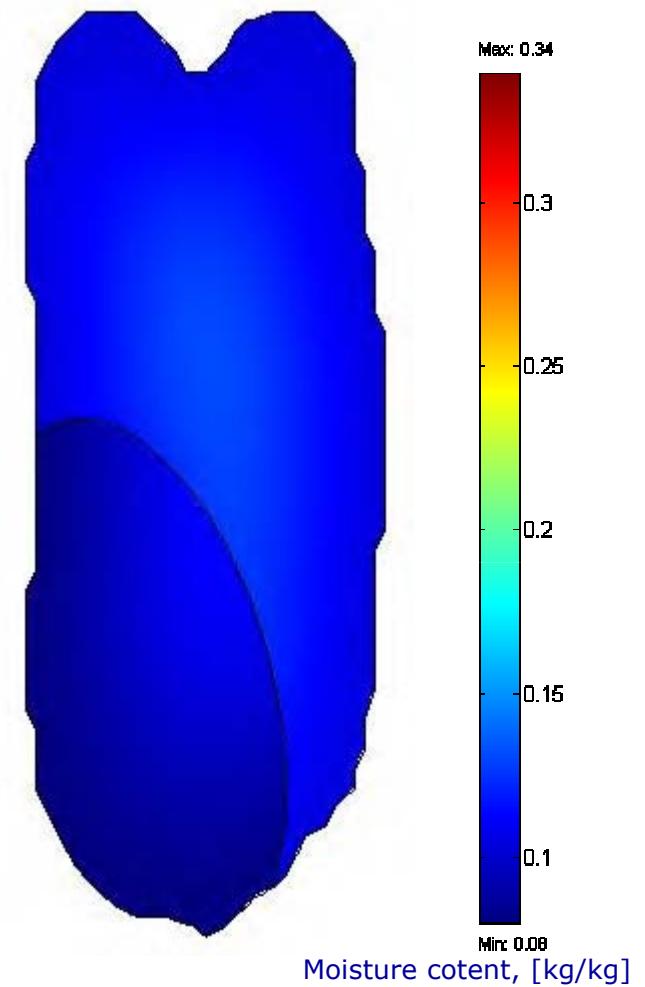
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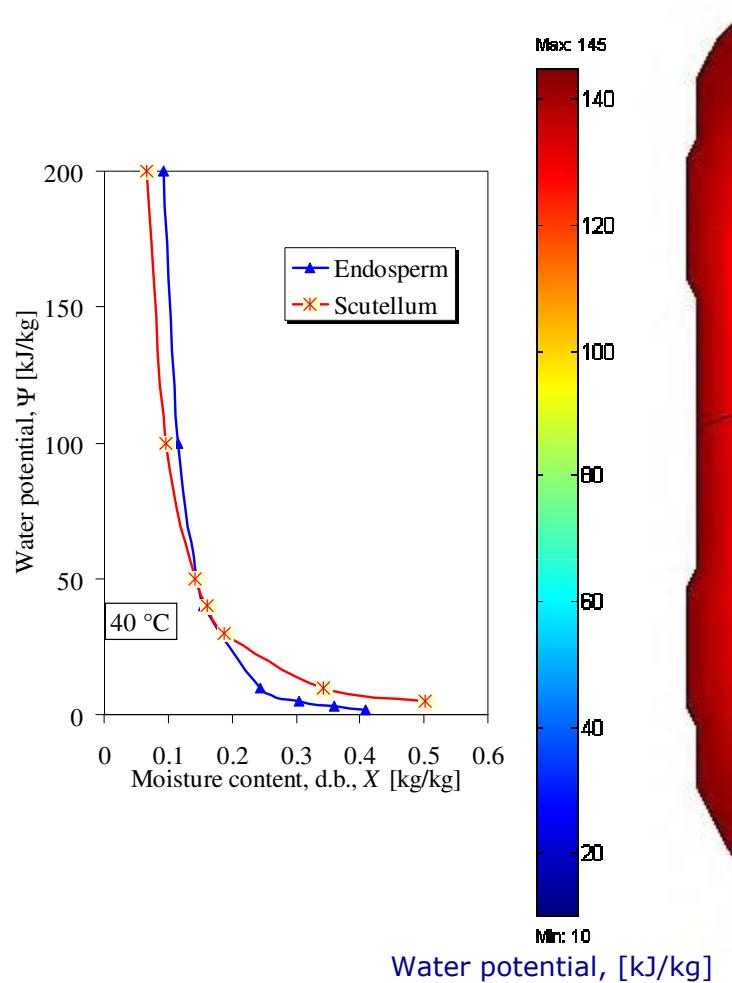
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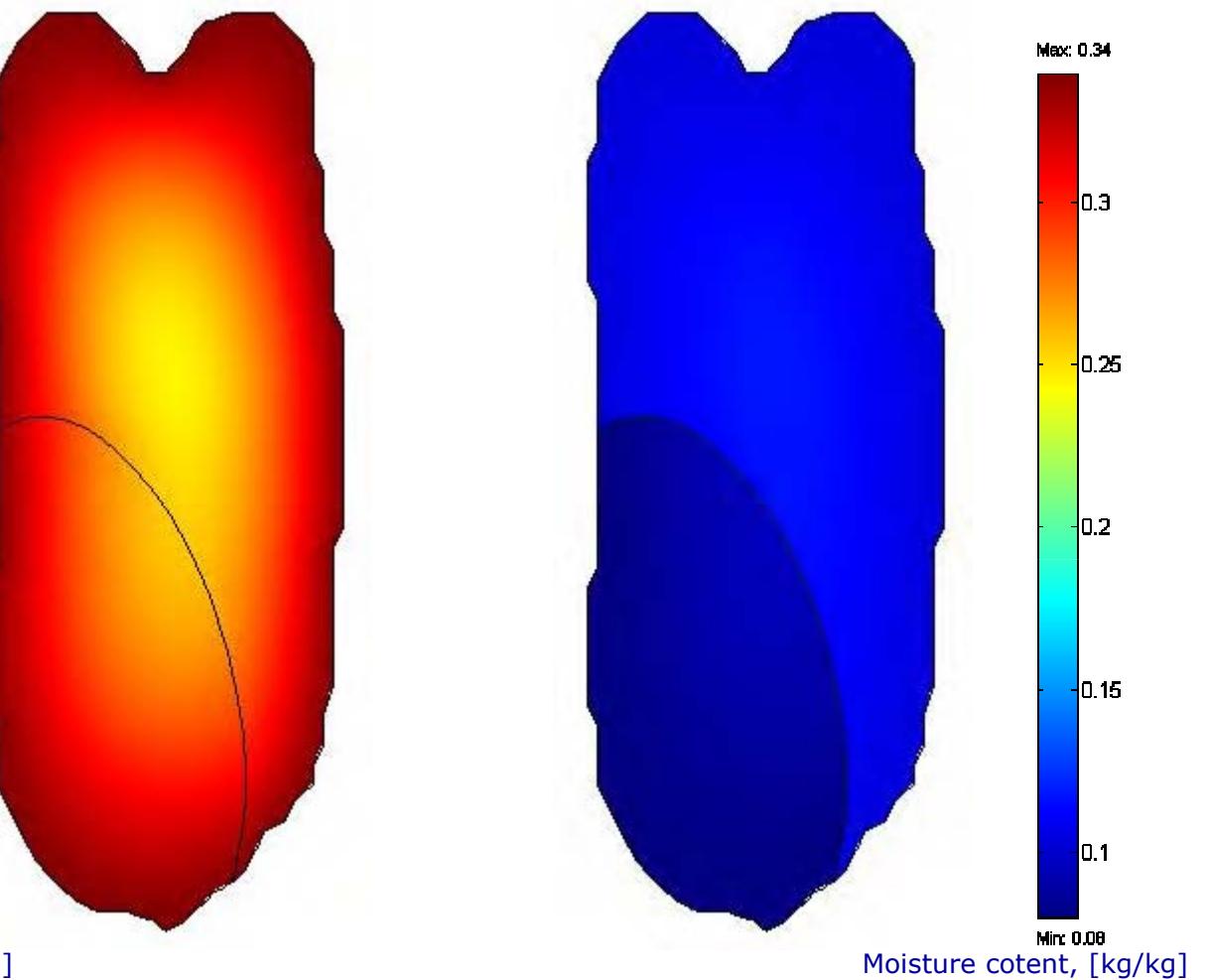
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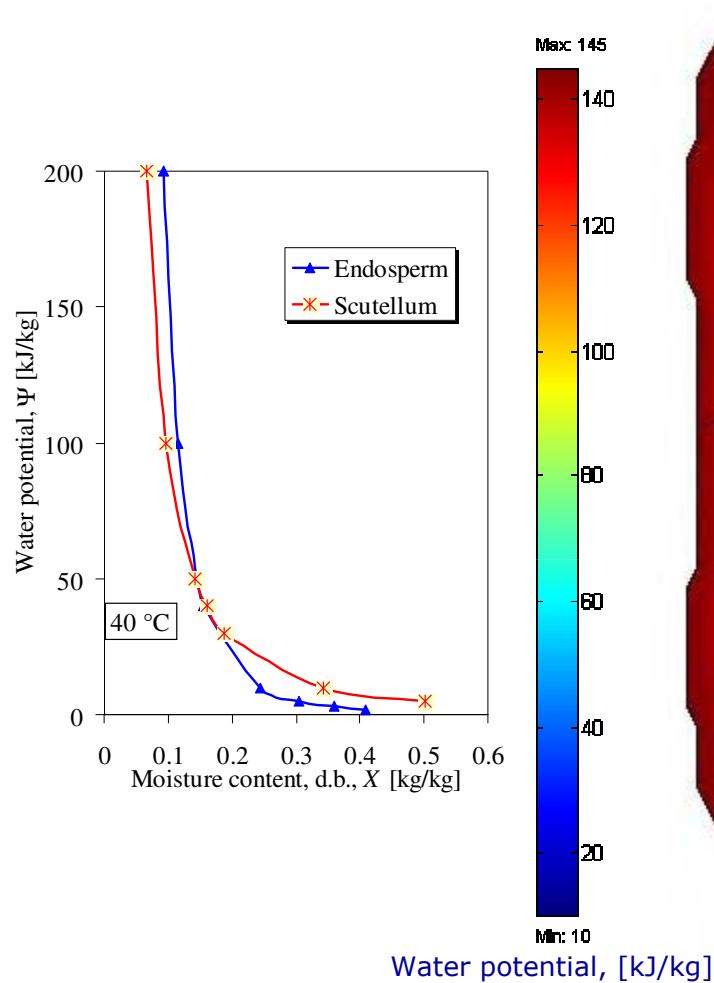
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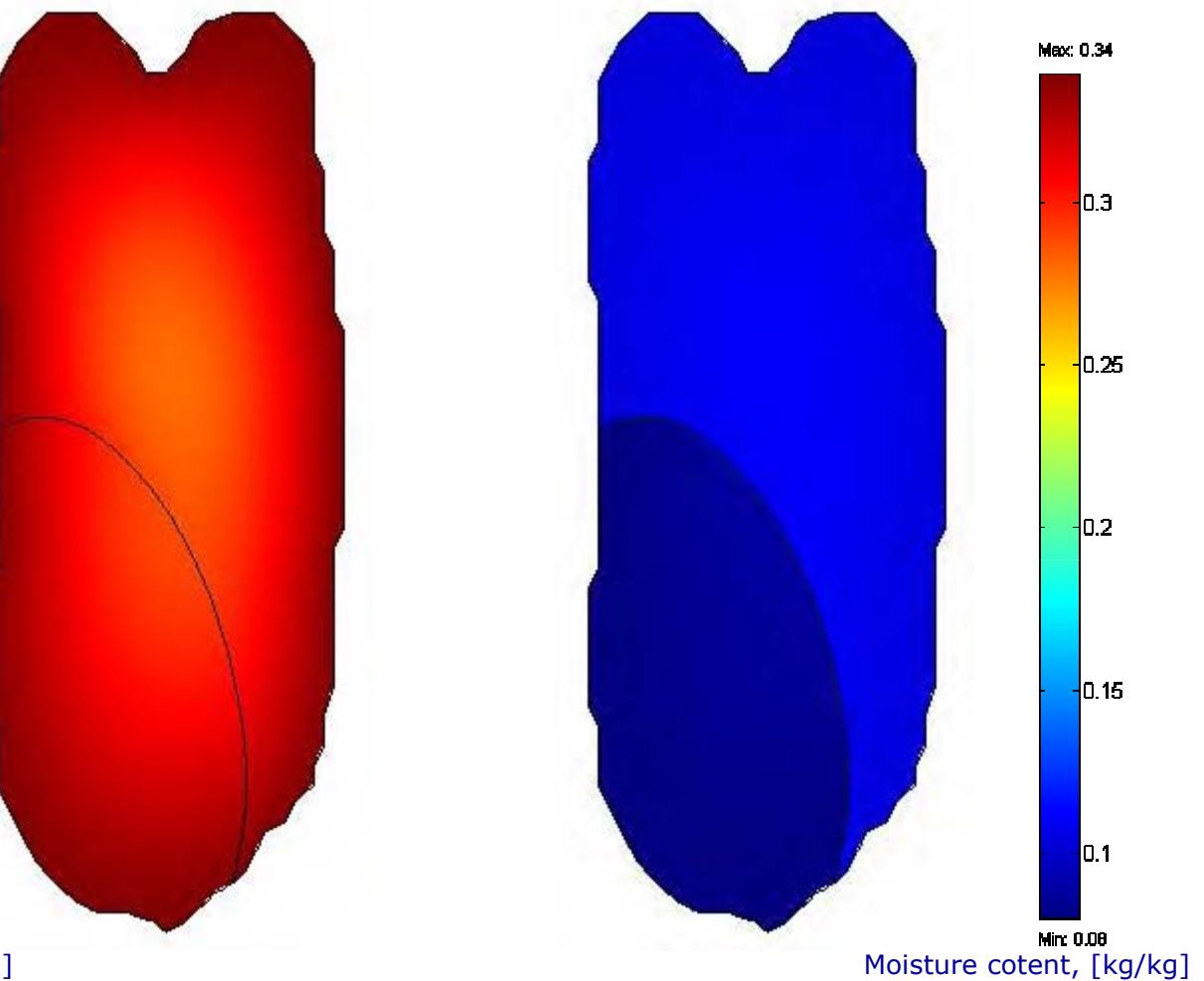
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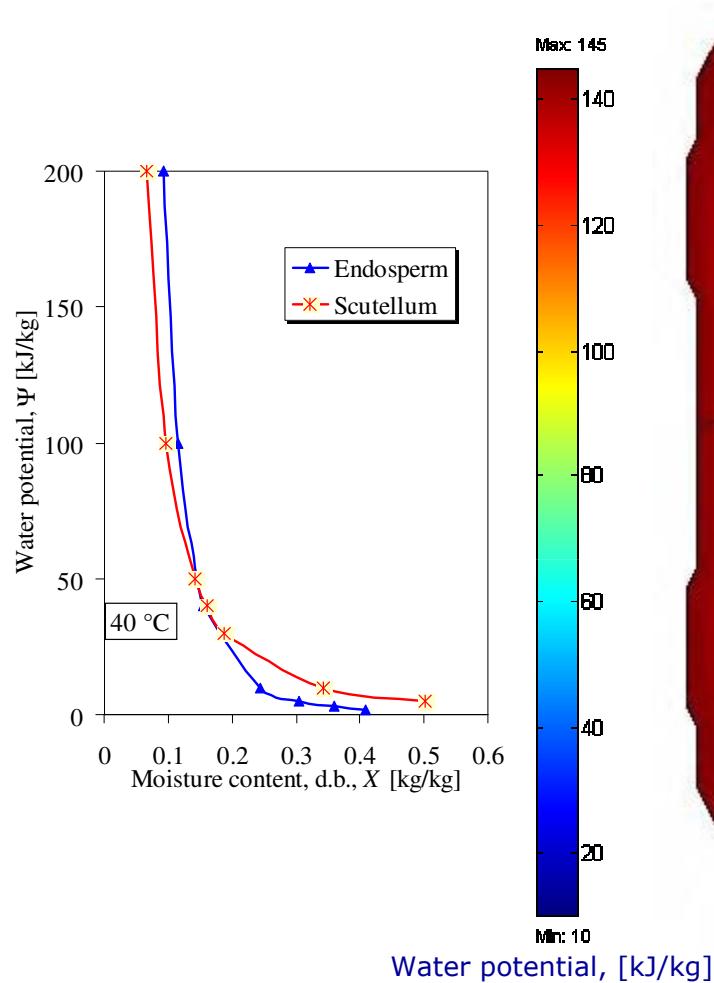
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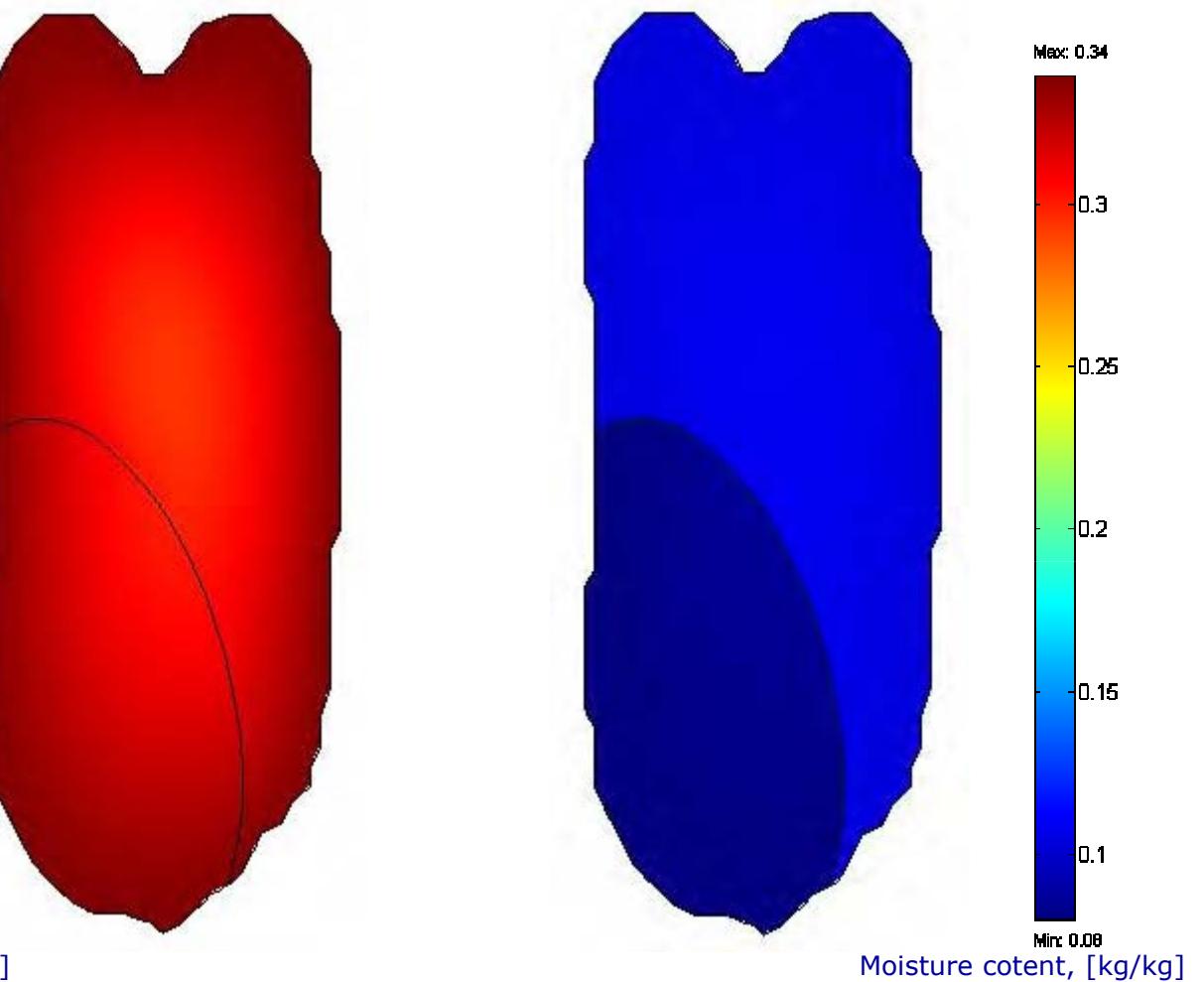
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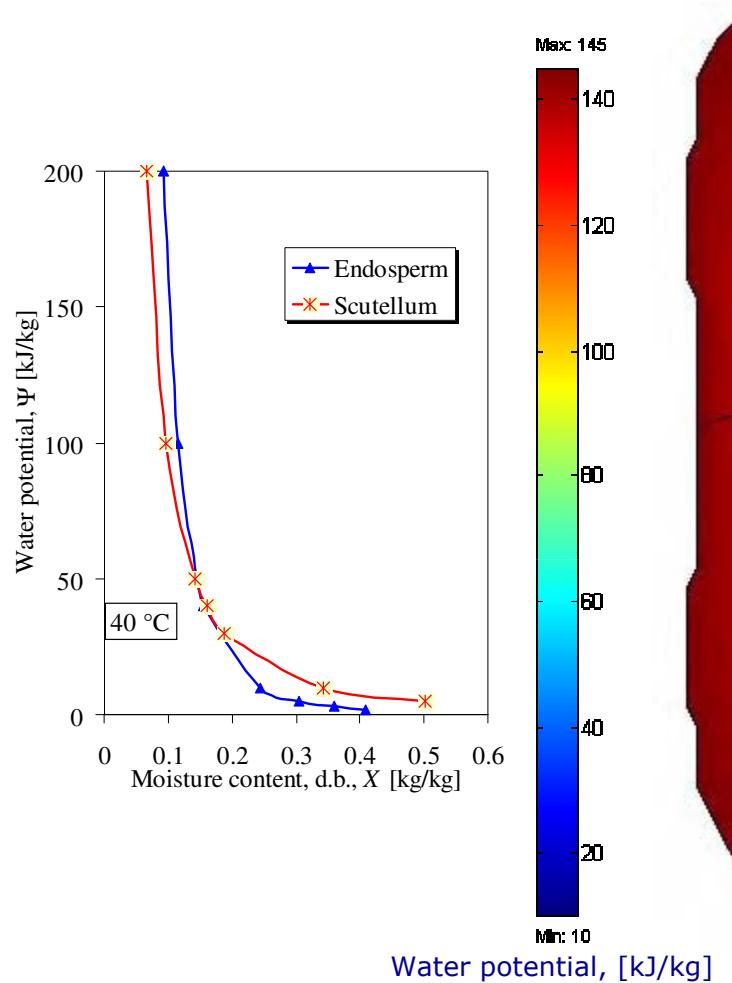
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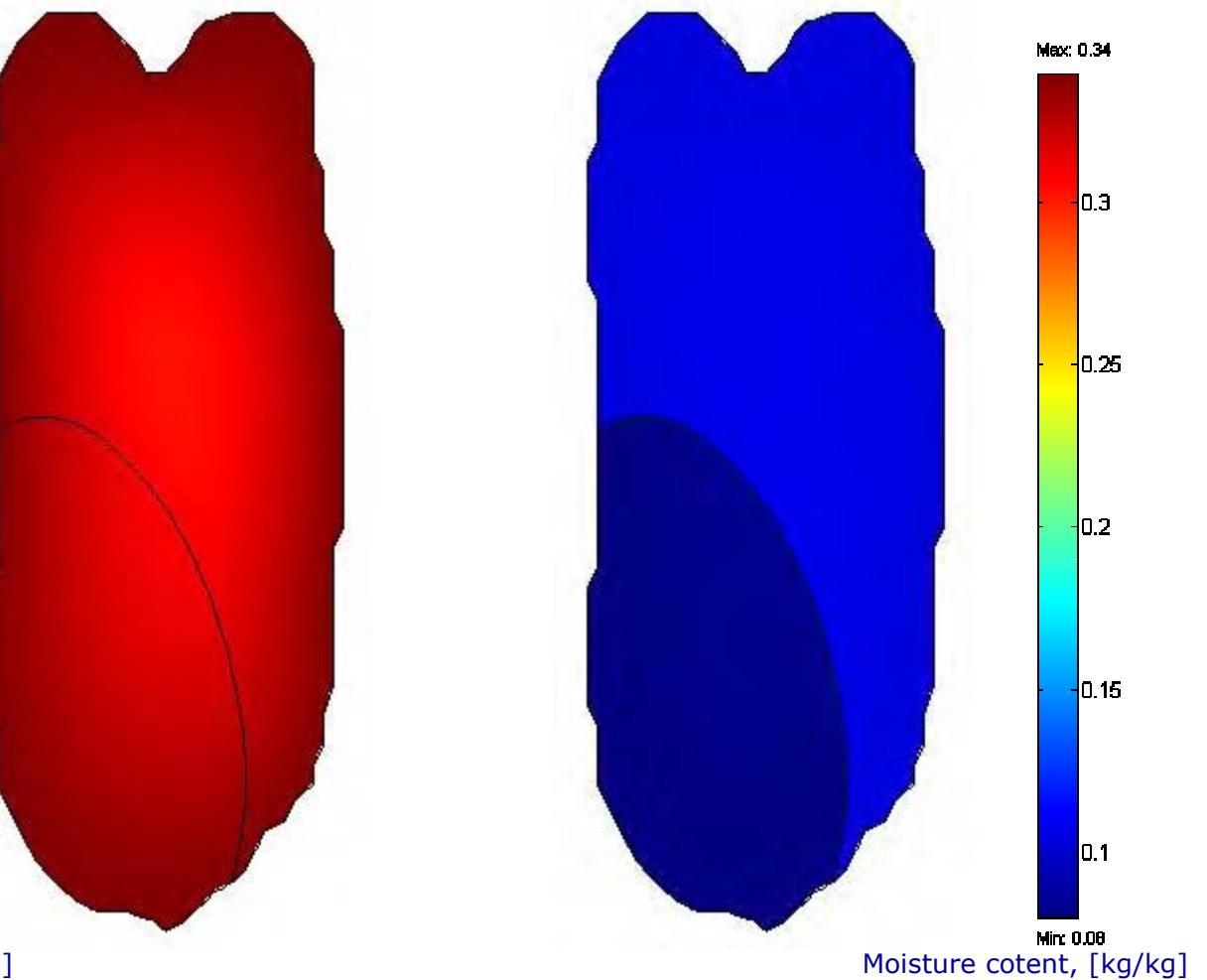
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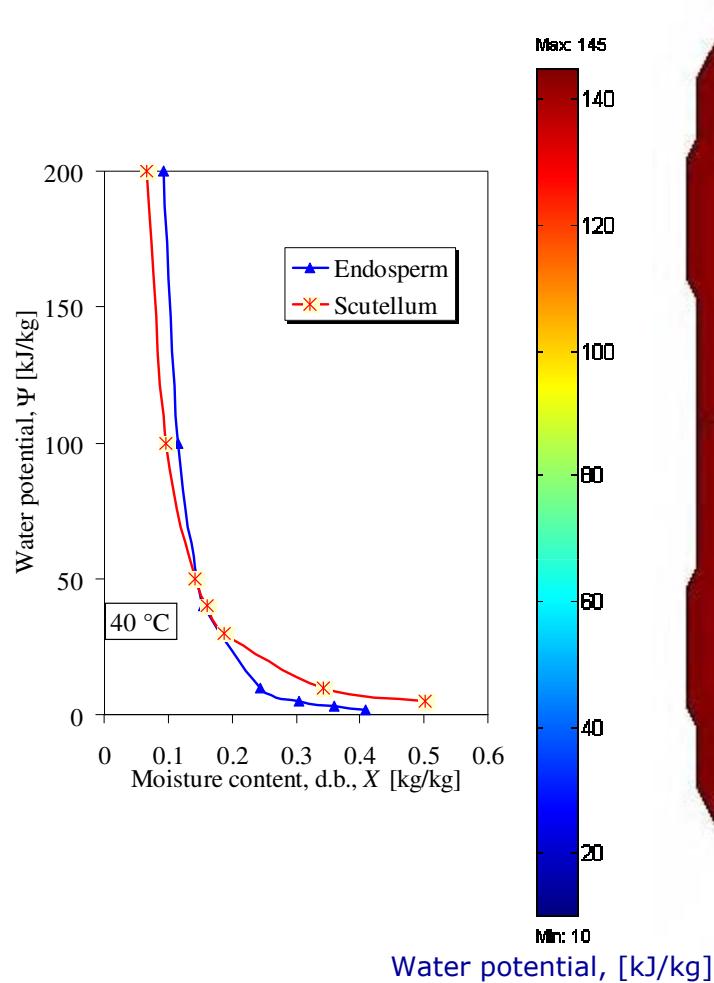
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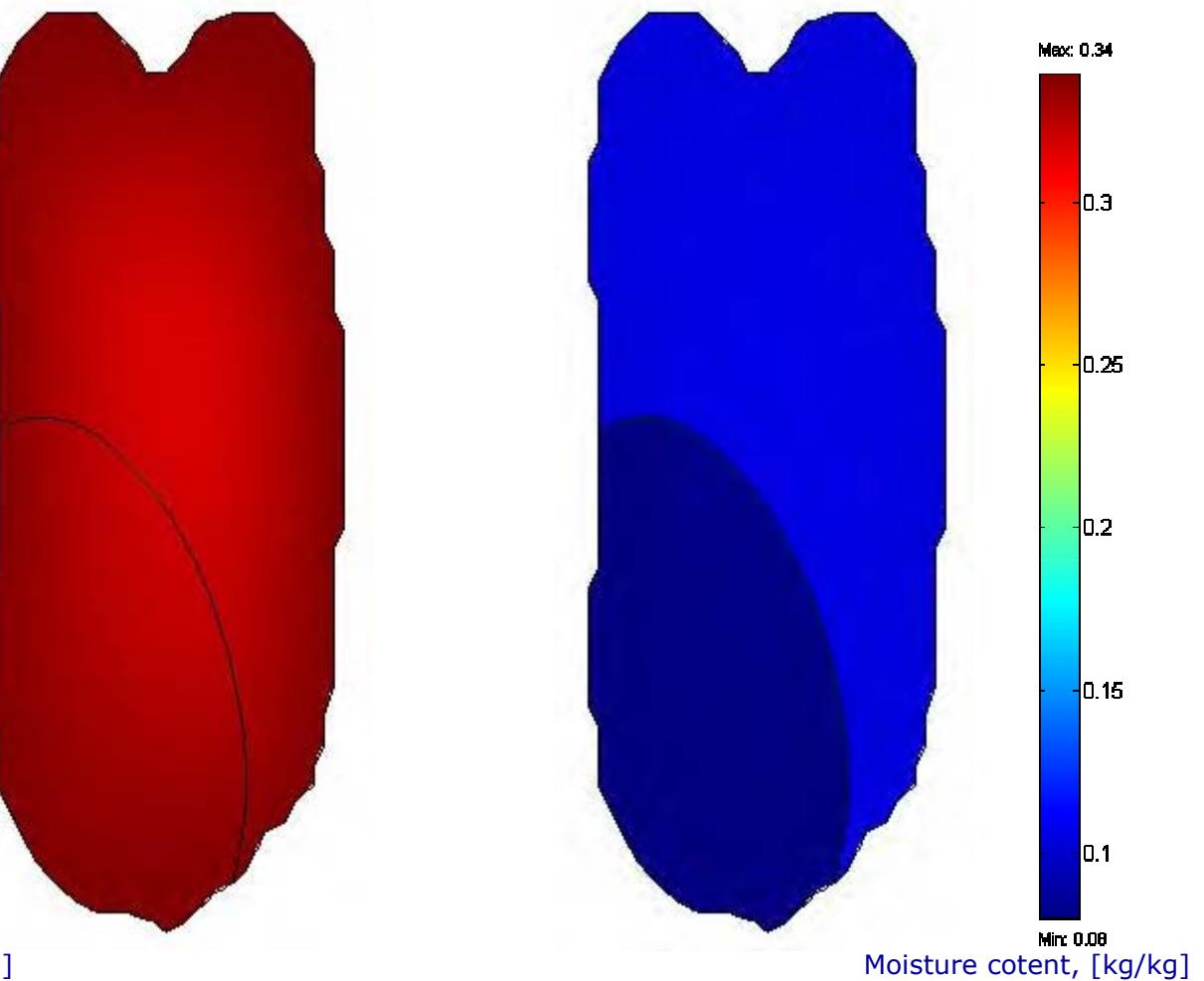
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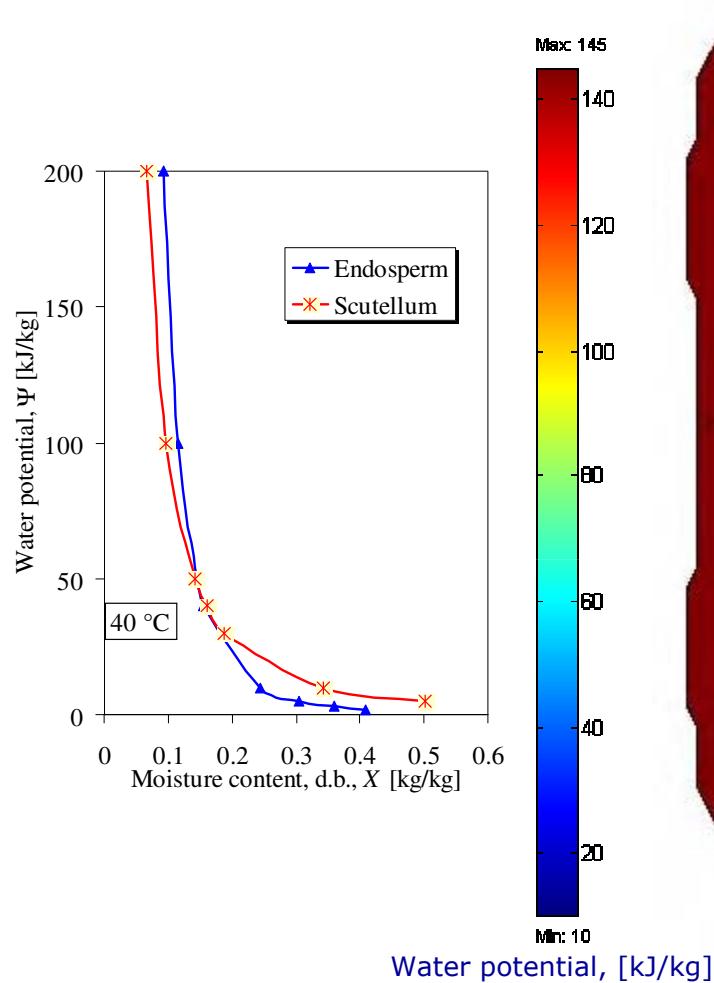
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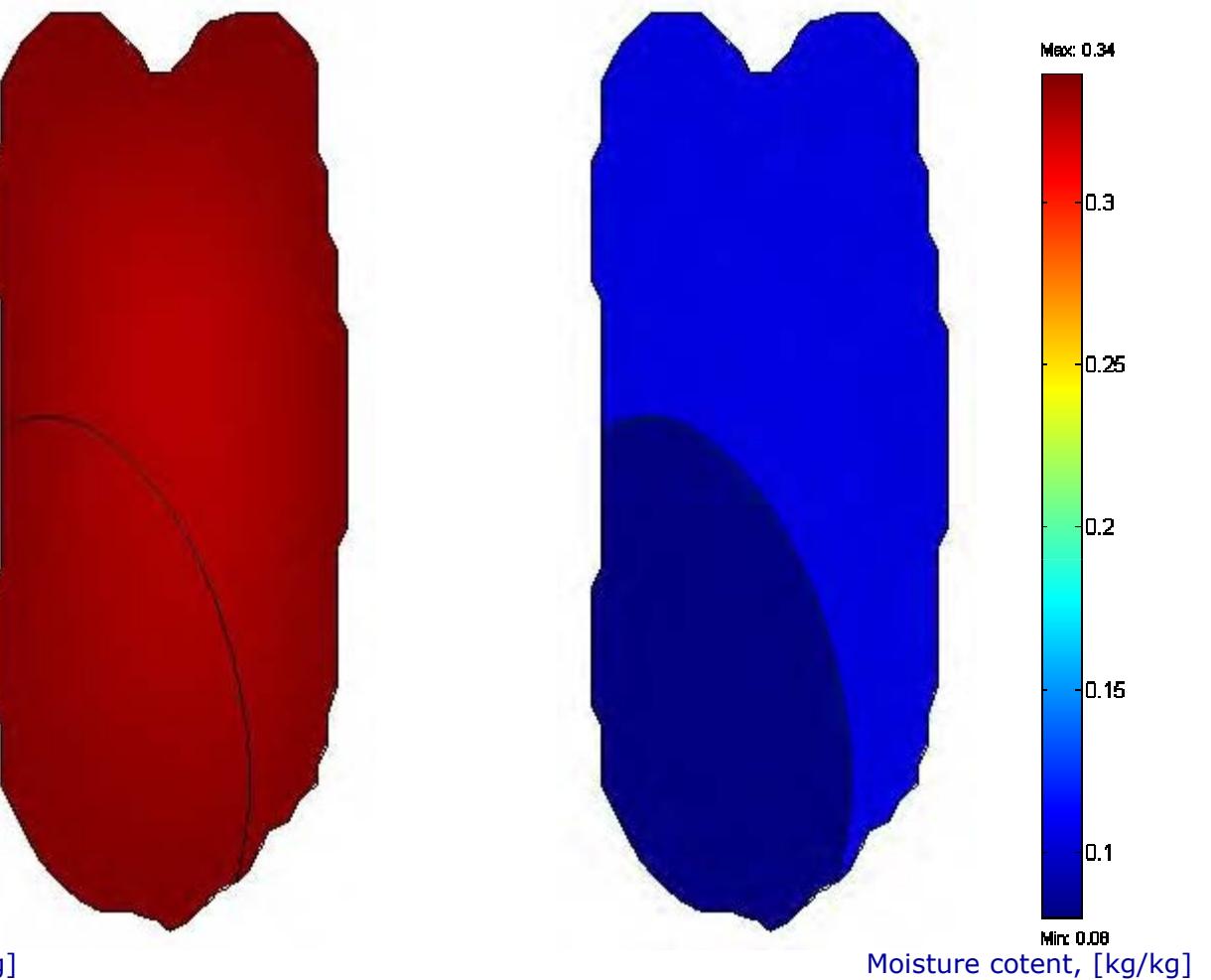
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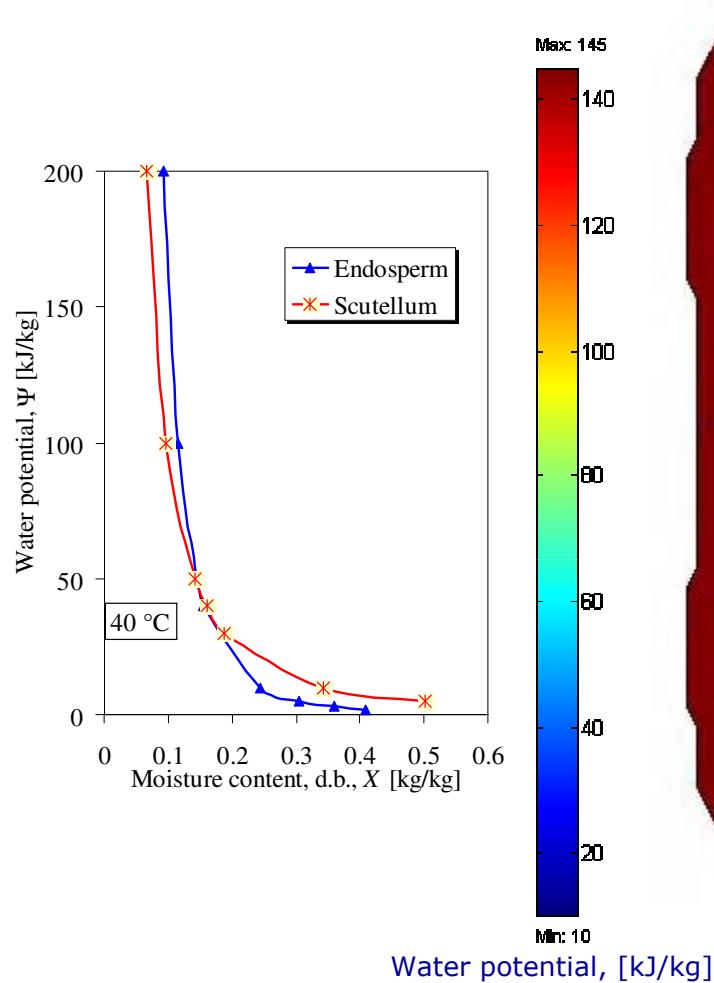
X changes based on grad Ψ



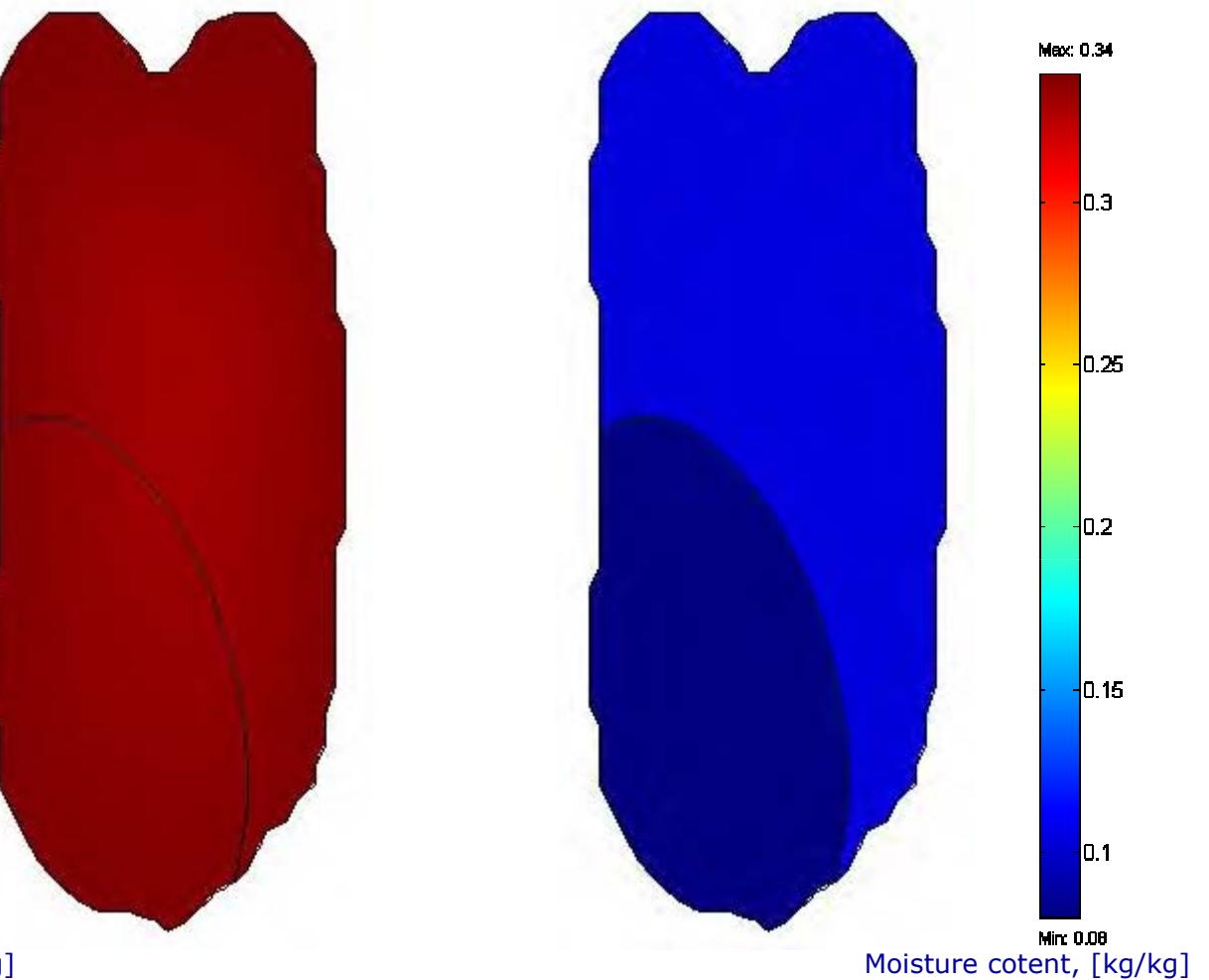
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Modelled Ψ changes



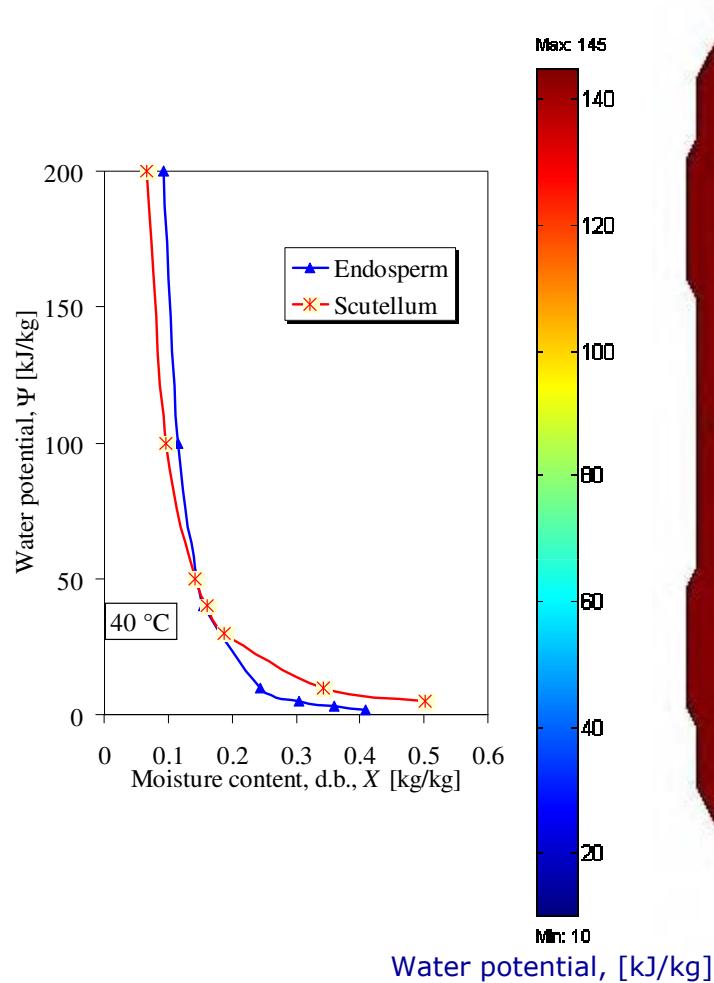
X changes based on grad Ψ



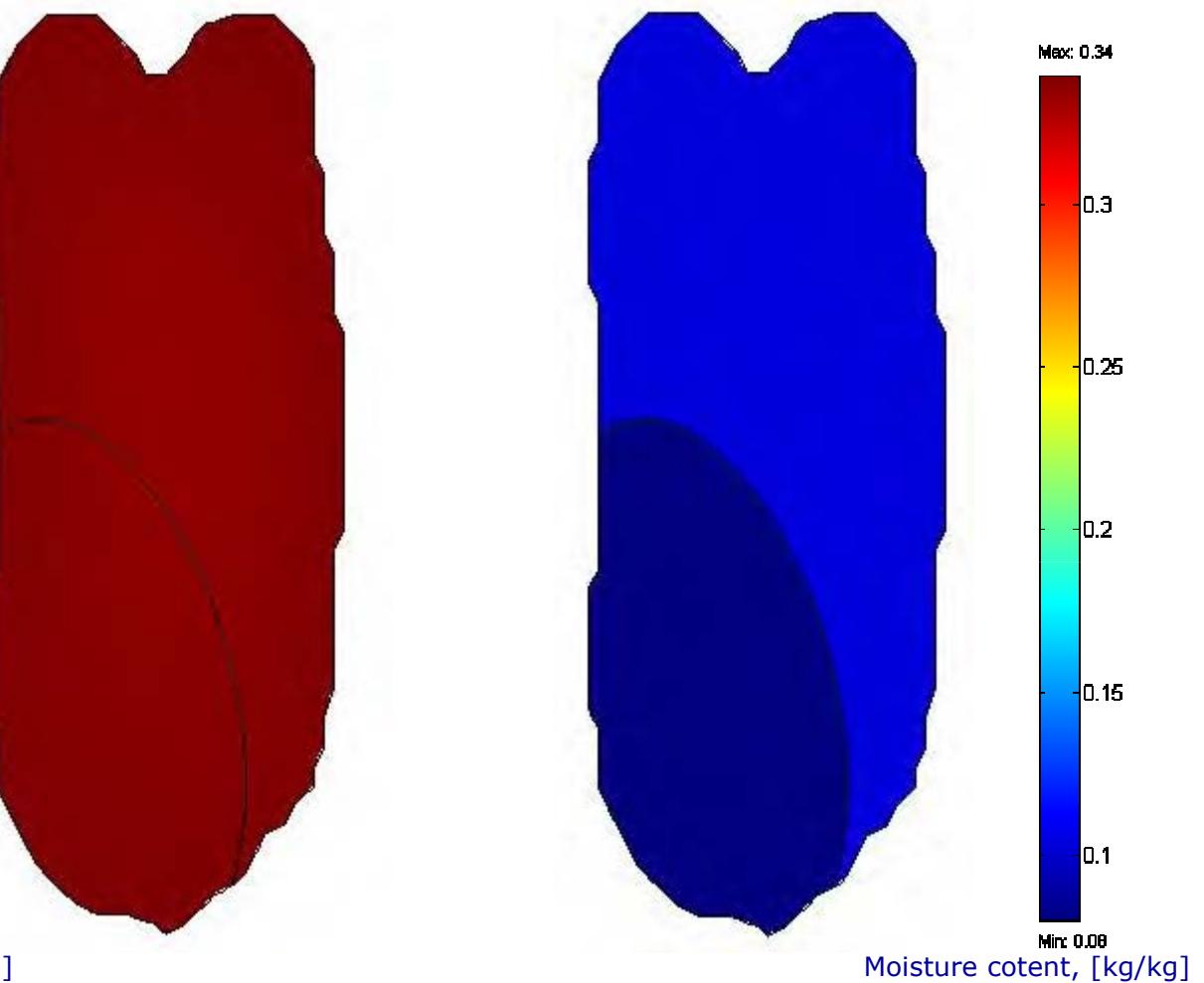
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Modelled Ψ changes



X changes based on grad Ψ



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CONCLUSIONS

- In the governing equation using water potential as the driving force has exact physical meaning, instead of the moisture gradient drying force.
- One multiphysical equation system gives more accurate solutions instead of iteration solutions.
- Further studies needs to be done to determine water potential above hygroscopic moisture content.



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THANK YOU FOR YOUR ATTENTION!



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